

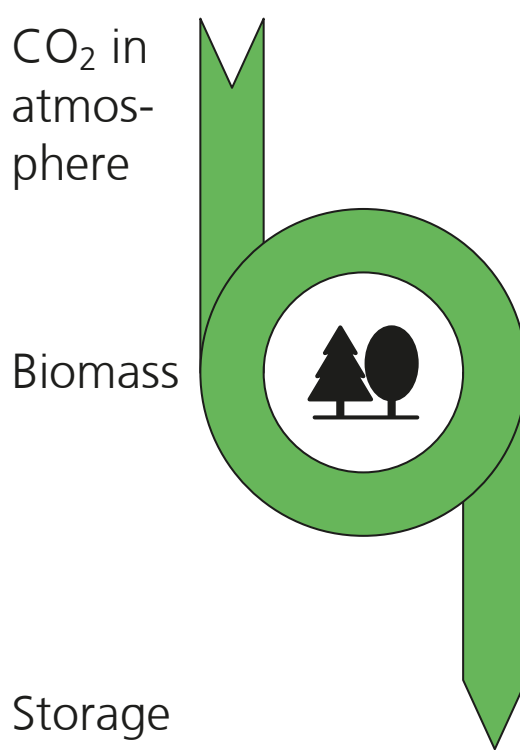
# CO<sub>2</sub> Capture from Combustion of Biomass Volatiles with a Chemical-Looping Combustion Process

Patrick Moldenhauer\*, Max Biermann, Tobias Mattisson, Carl Linderholm†  
Chalmers University of Technology, Division of Energy Technology, Gothenburg, Sweden

\* Corresponding author (patrick.moldenhauer@chalmers.se)  
† Presenting author (carl.linderholm@chalmers.se)



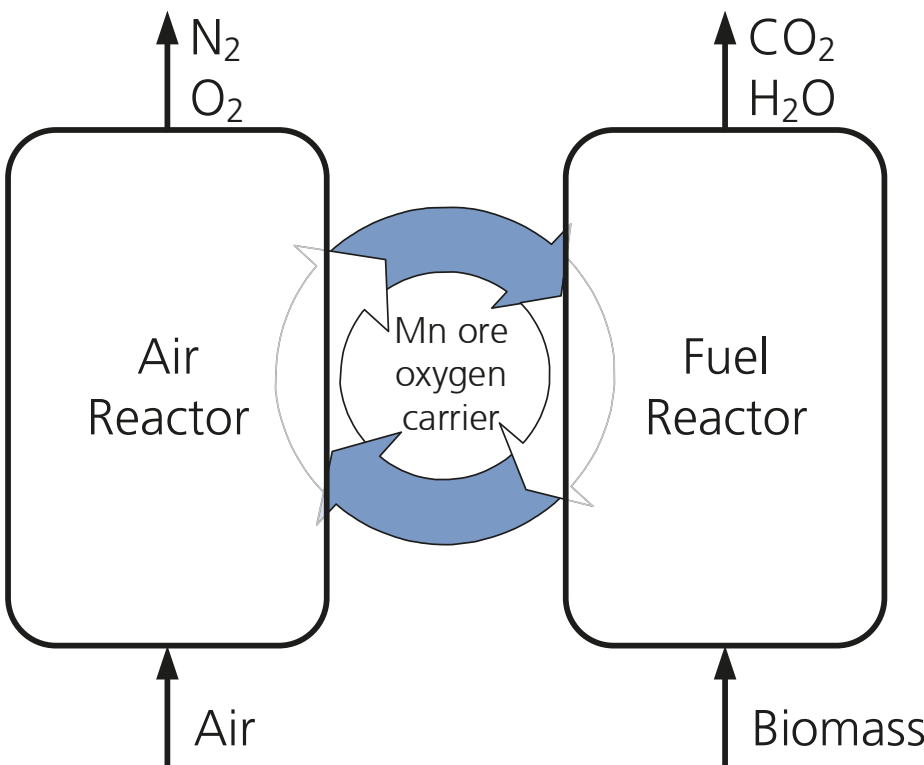
## Summary



Capture and storage of CO<sub>2</sub> from combustion of biomass, i.e., bio-energy carbon capture and storage (BECCS), makes it possible to obtain so-called negative emissions – the atmosphere is cleansed from carbon dioxide. In this study, five manganese ores are investigated as oxygen carriers in chemical-looping combustion of biomass fuels. A laboratory-scale chemical-looping combustion (CLC) system was used, which has a nominal fuel input of 300 W<sub>th</sub>. The aims were to investigate the reactivity of these oxygen carriers towards biomass fuels as well as their mechanical stability. A synthetic “biomass volatiles” gas – representing the gas generated during devolatilization of a wood-based fuel – was used as fuel in this study, and it was studied how the different gas components react with the oxygen-carrier particles. Additional experiments were conducted with methane and a syngas. Parameter studies concerning temperature and specific fuel-reactor bed mass (in kg/MW<sub>th</sub>) were carried out. With the synthetic biomass volatiles, conversion of fuel carbon to CO<sub>2</sub> as high as 97.6% was achieved. For a majority of the investigated ores, essentially all C2 and C3 hydrocarbons were converted, as well as a very high fraction of the CO. Reactivity towards CH<sub>4</sub> on the other hand was generally lower, but improved at higher temperatures.

## Chemical-looping combustion

- Two interconnected fluidized-bed reactors
- No exchange of gas between reactors, i.e., air and fuel are not mixed.
- Oxygen is transported to the fuel by a solid oxygen carrier, which is cyclically oxidized and reduced.
- Net heat of reaction is the same as for regular air combustion, i.e., there is no energy penalty for separation of CO<sub>2</sub>.



## Conclusions

- It is possible to remove CO<sub>2</sub> efficiently from the atmosphere through a chemical-looping combustion process with biomass as fuel. The use of manganese ores has the potential to keep the costs of the CLC process low.
- The properties of the five manganese ores investigated differed significantly and, hence, it is likely that other ores exist that are even better suited.
- The attrition resistance of two of the materials was higher than for the other Mn ores tested. Their attrition was similar to that of ilmenite (Fe-Ti-based mineral).
- All of the manganese ores also showed oxygen uncoupling, which could be an advantage in large boilers, with inadequate mixing.

## Result

	Mechanical attrition	Redox attrition	Biomass reactivity	Methane reactivity	Syngas reactivity
Elwaleed C	--	+	+	–	+
Tshipi	○	--	+	n/a	++
Gui Zhou	+	++	+	○	++
Braunite	+	+	○	–	++
Morro da Mina	+	–	–	n/a	n/a
+ favorable property      ○ average property      – unfavorable property					

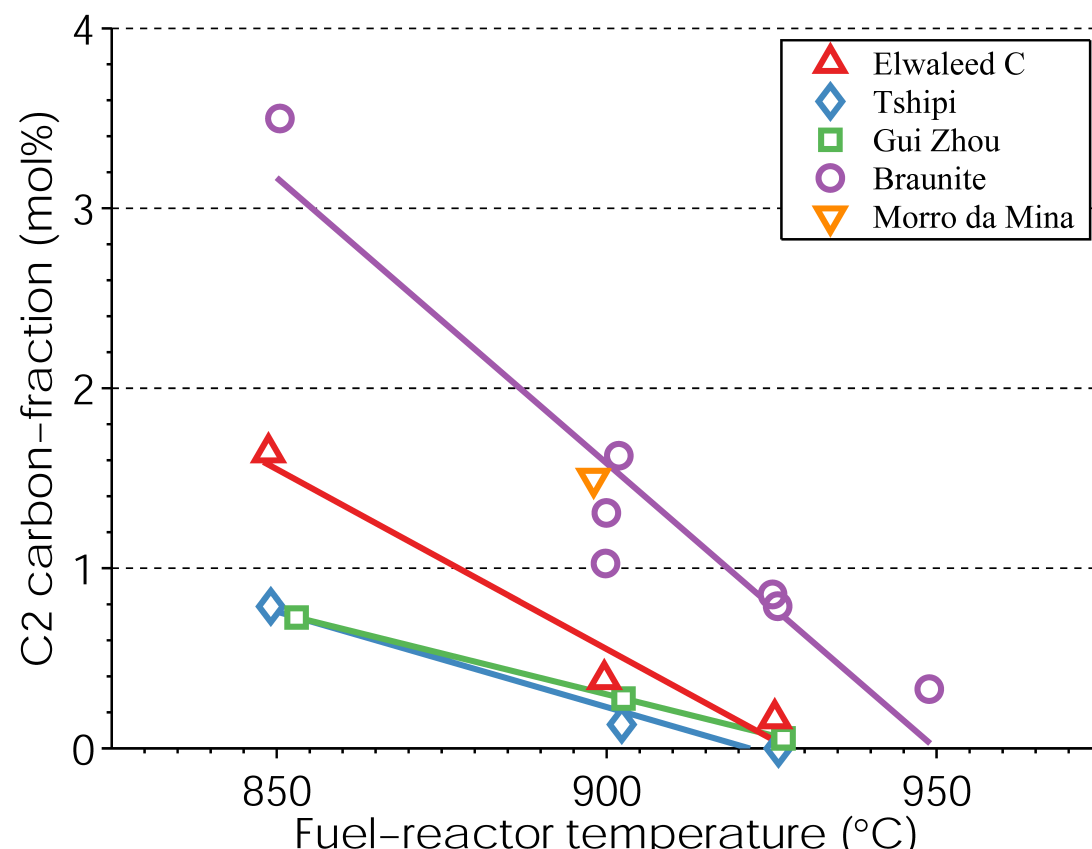
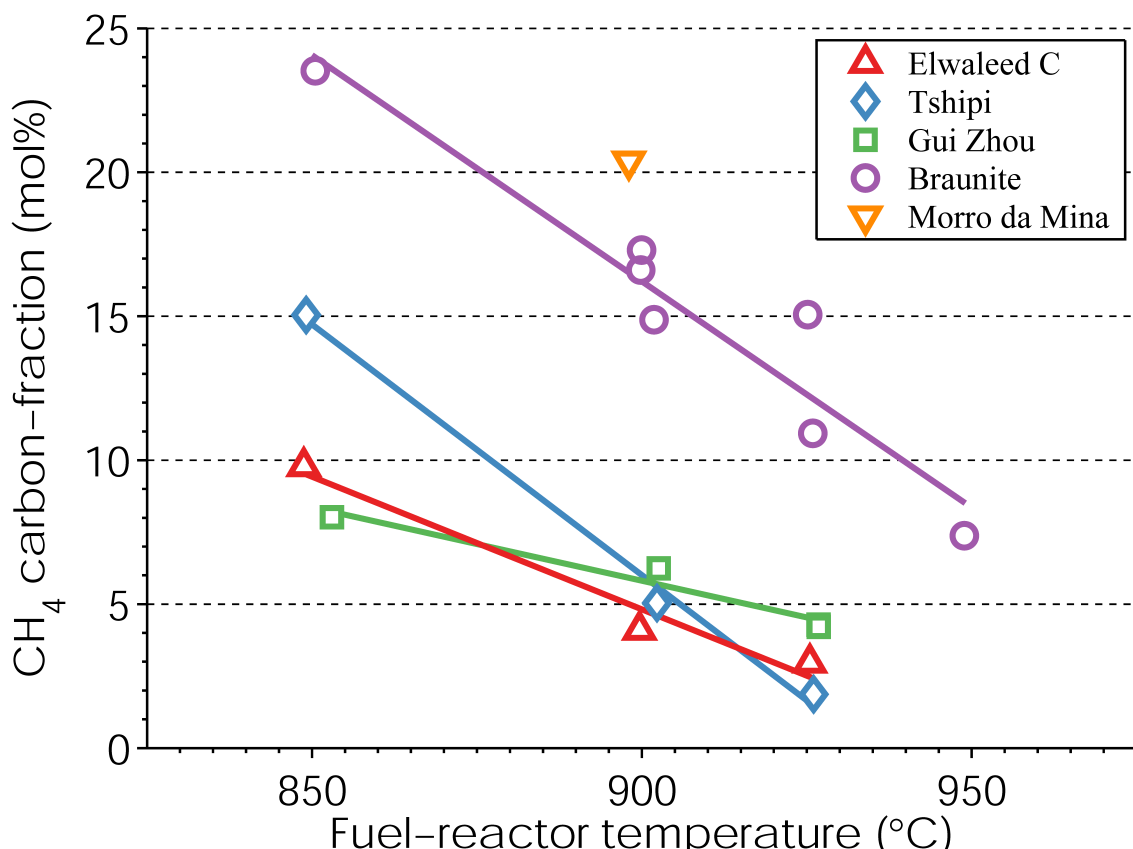
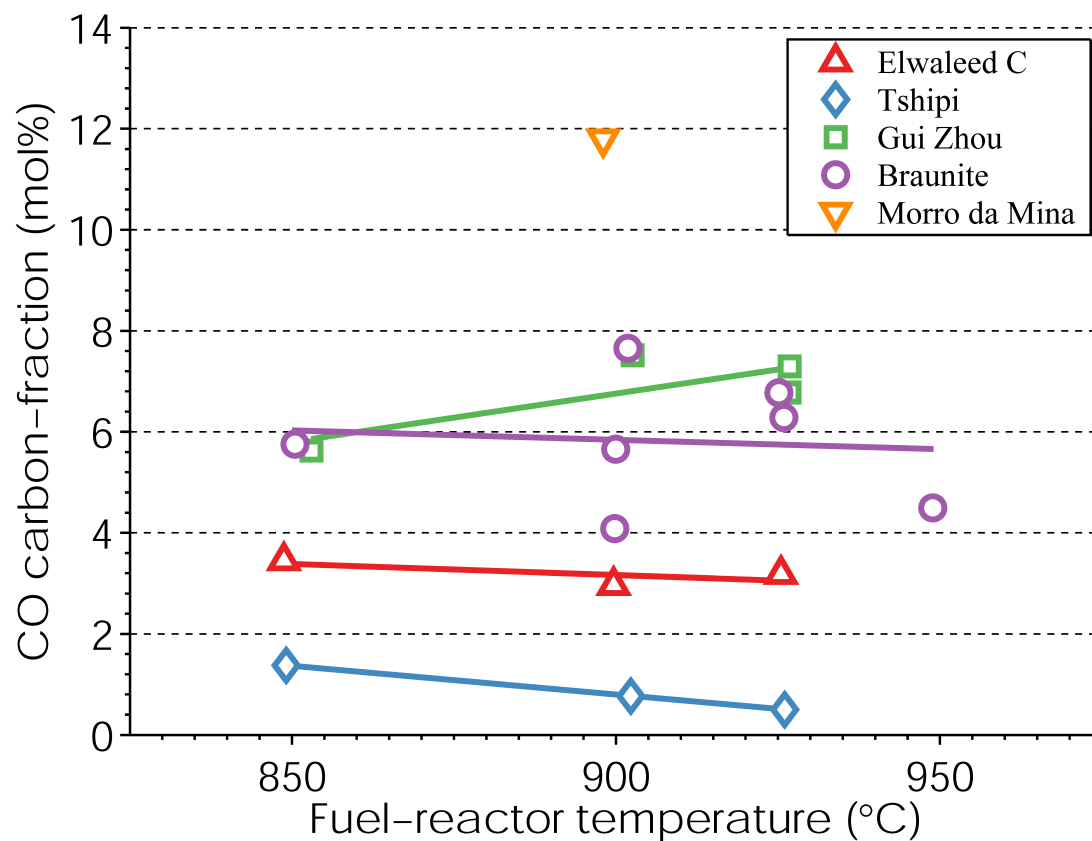
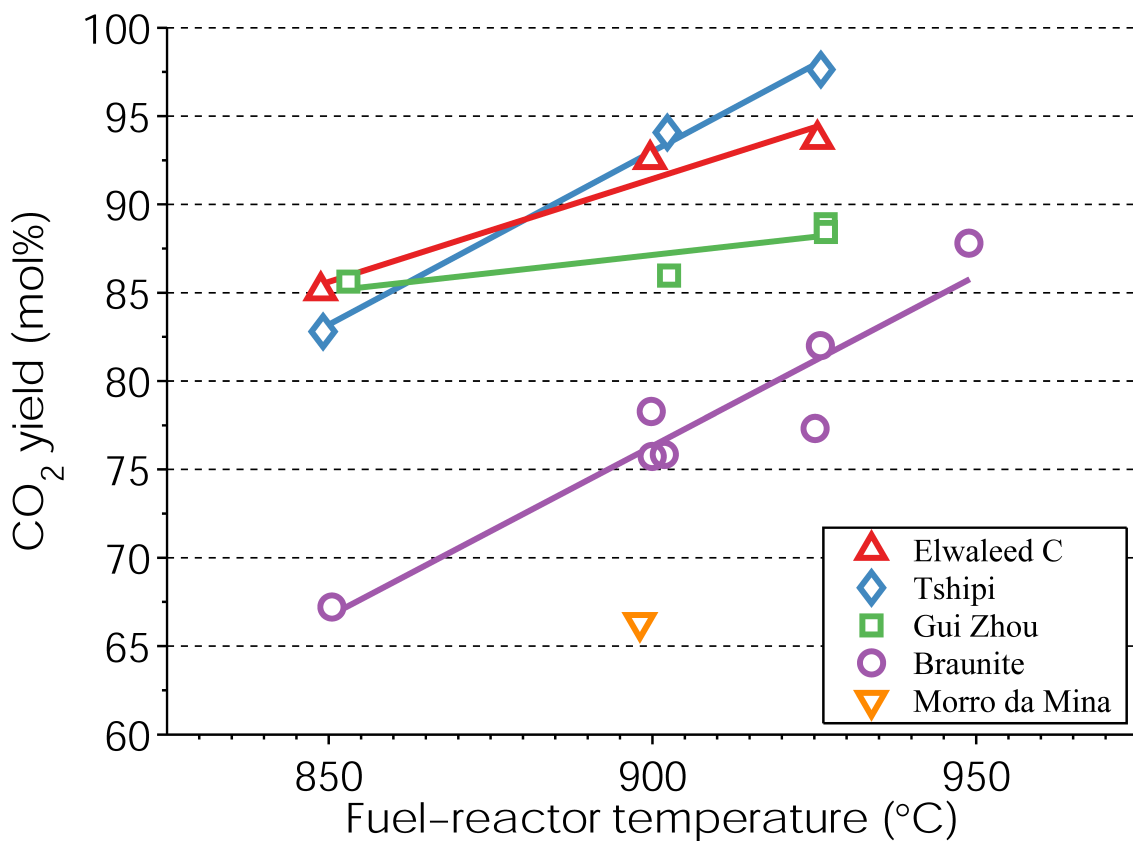
### Key results summarized (table above)

- Gui Zhou Mn ore has the best overall properties.
- All ores tested have higher reactivity towards CO than towards CH<sub>4</sub>.
- Attrition under redox condition differs from mechanical attrition. Redox attrition is more significant.

### Fuel conversion (figures below)

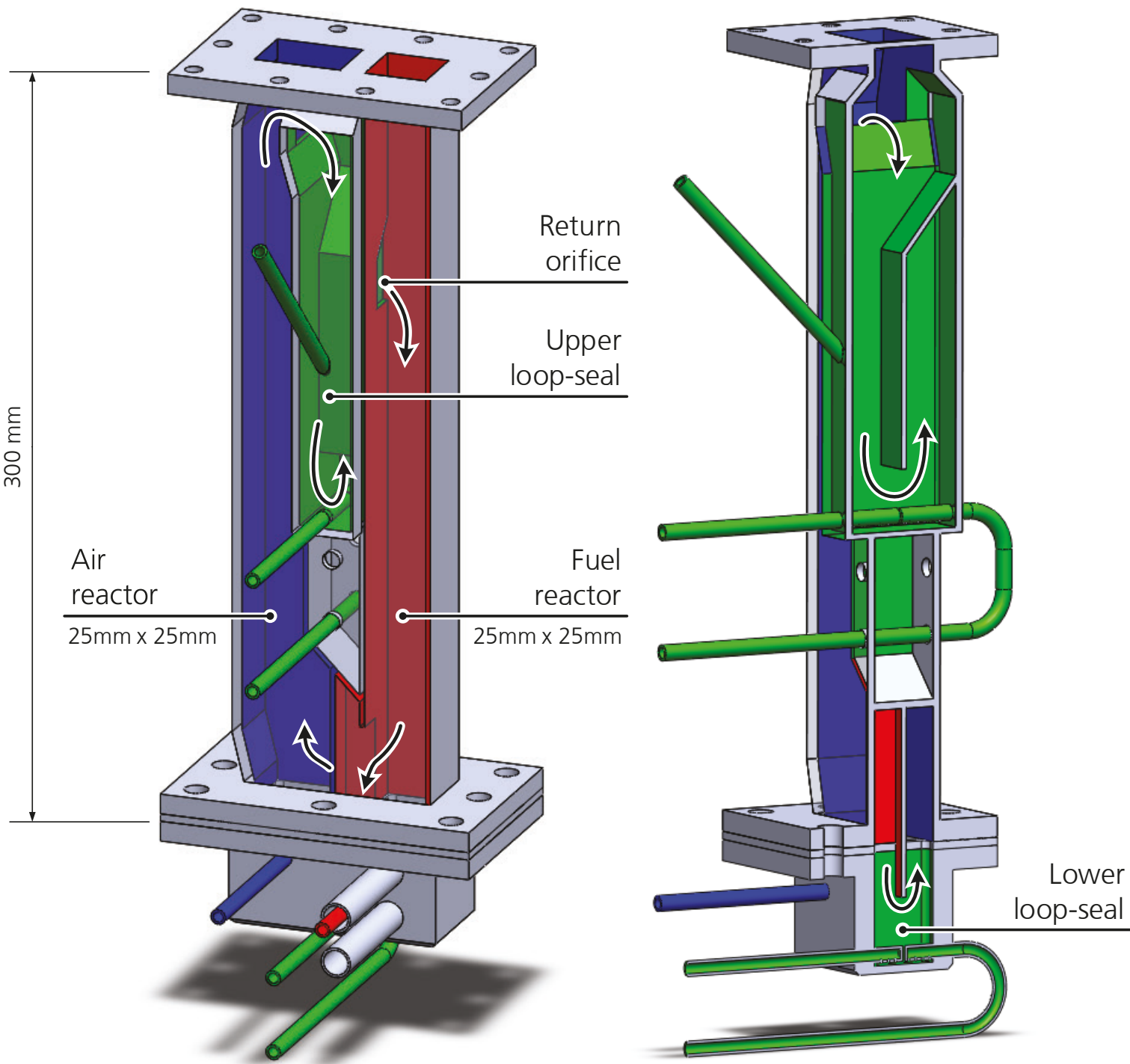
CO<sub>2</sub> yield/carbon fractions: molar amount of fuel carbon converted to CO<sub>2</sub>/CO, CH<sub>4</sub> or C<sub>2</sub>.

- No C3-species were detected within the conditions investigated.
- Strong decrease of CH<sub>4</sub> and C<sub>2</sub> when increasing temperature.
- No clear temperature trend for CO fraction as long as CH<sub>4</sub> and C<sub>2</sub> exist. CO is probably an intermediate reaction product.
- Clear increase in CO<sub>2</sub> yield when increasing temperature.



Fuel conversion

## Experimental details



300 W chemical-looping reactor

	CLOU	→ Biomass volatiles	→ Methane	→ Syngas (CO/H <sub>2</sub> )	→ CLOU
Elwaleed C	×	15 h	4 h	9 h	×
Tshipi	×	14 h	n/a	3 h	n/a
Gui Zhou	×	11 h	15 h	6 h	n/a
Braunite	×	16 h	3 h	10 h	×
Morro da Mina	×	7 h	n/a	n/a	n/a

Experiments

Component	Fraction (vol%)	Carbon fraction (atomic %)	LHV (MJ/m <sup>3</sup> )
CO	43	55.1	12.6
H <sub>2</sub>	30	–	10.8
CH <sub>4</sub>	20	25.6	35.8
C <sub>2</sub> H <sub>4</sub>	6	15.4	59.0
C <sub>3</sub> H <sub>6</sub>	1	3.8	85.9
Total	100	99.9	20.2

Fuel composition



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