



## Evidence for an Unusual Temperature Dependence of the Atmospheric Corrosion of Zinc

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The atmospheric corrosion behavior of zinc in the presence of NaCl has been investigated using well-controlled laboratory exposures in 95% RH air at ten different temperatures in the range  $-4$  to  $22^\circ\text{C}$ . Results show that a critical temperature ( $\sim -0.5^\circ\text{C}$ ) exists in zinc corrosion above which the rate of corrosion is constant/independent of temperature, and, below which there is a positive correlation between temperature and corrosion rate. The corrosion products formed above and below  $-0.5^\circ\text{C}$  are also entirely different. While simonkolleite, hydrozincite and zinc carbonate hydroxide are the main corrosion products at  $T \geq -0.5^\circ\text{C}$ , the same compounds are absent at  $T < -0.5^\circ\text{C}$ . Instead, sodium zinc carbonate ( $\text{Na}_2\text{Zn}_3(\text{CO}_3)_4 \cdot 3\text{H}_2\text{O}$ ) is the dominant corrosion product at low temperature, together with  $\text{Na}_2\text{ZnCl}_4 \cdot 3\text{H}_2\text{O}$  and sweetite ( $\text{Zn}(\text{OH})_2$ ). The results are interpreted in terms of two distinct corrosion modes prevailing at “high” and “low” temperature, respectively.

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Manuscript submitted September 8, 2016; revised manuscript received October 31, 2016. Published November 8, 2016.

Zinc (Zn) is used for galvanizing steel to mitigate corrosion. Also, rolled Zn ( $< 1\%$  Cu), die-cast Zn-Al (4% Al), and brass (Cu + 20–40% Zn) have numerous applications in e.g., infrastructure and engineering sectors,<sup>1–4</sup> where environmental degradation is often an issue. Thus, Zn corrosion has been studied by means of atmospheric corrosion exposures in the field,<sup>5–7</sup> and in the laboratory,<sup>8–10</sup> as well as, in the presence of an aqueous media using droplets,<sup>11,12</sup> and bulk electrolyte exposures.<sup>13</sup> Various aspects of Zn corrosion have been studied in the works cited above and other reports.

When zinc is exposed to the atmosphere in the presence of chloride, the main corrosion products are reported to be simonkolleite ( $\text{Zn}_5(\text{OH})_8\text{Cl}_2\text{H}_2\text{O}$ ) and hydrozincite ( $\text{Zn}_5(\text{CO}_3)_2(\text{OH})_6$ ).<sup>14–18</sup> Zinc hydroxy sulfates, e.g.,  $\text{ZnSO}_4 \cdot 3\text{Zn}(\text{OH})_2 \cdot 4\text{H}_2\text{O}$ , often occur in environments containing traces of  $\text{SO}_2$ .<sup>19</sup> There are studies examining the importance of cations in the salt-induced atmospheric corrosion of Zn. For instance, Lindström et al.<sup>21</sup> studied the corrosivity of chloride and sulfate salts toward Zn at  $22^\circ\text{C}$  and noted that sodium-containing salts were much more corrosive compared to salt containing e.g.,  $\text{Mg}^+$ ,  $\text{Zn}^{2+}$ , and  $\text{NH}_4^+$ . Similarly, Sanyal et al.<sup>20</sup> examined the atmospheric corrosion of Zn at  $40^\circ\text{C}$  and 85% relative humidity (RH) in the presence of different salts. Thomas et al.<sup>22–26</sup> have investigated the Zn corrosion as a function of pH in NaCl(aq) solution,<sup>22</sup> reported on the corrosion layers/products formed in contact with a seawater droplet,<sup>23</sup> and reported on the occurrence of the oxygen reduction reaction (ORR) on Zn oxide.<sup>24–26</sup> And finally, studies have shown that the role played by the microstructure is vital in the case of Zn alloy-coated steels.<sup>27–30</sup> As an example, Prosek et al.<sup>27</sup> reported that a finer microstructure resulted in better corrosion resistance in Zn-5Al and Zn-3Al-2Mg alloys and attributed this to a rapid blocking of cathodic sites.

While all the above-mentioned studies have been performed at ambient temperature or higher, Zn is often subjected to corrosive conditions at temperatures below ambient. For example, because of the use of de-icing salt (NaCl) on the roads during winter in temperate and cold regions of the world, car bodies made of Zn-coated (galvanized) steel are subjected to NaCl-induced atmospheric corrosion at temperatures close to or below  $0^\circ\text{C}$ .

Because the anodic and cathodic reactions and electrolytic conductivity are all thermally activated processes,<sup>31–33</sup> the rate of electrochemical corrosion usually increases with temperature. In atmo-

spheric corrosion, gases that are adsorbed on surfaces or dissolved in the surface electrolyte play important roles, i.e., as oxidants ( $\text{O}_2$ ) or by reacting with the surface film ( $\text{SO}_2$ ,  $\text{CO}_2$ ). Because gas adsorption and gas dissolution are exothermic processes, the equilibrium concentration of dissolved and adsorbed gases increases with decreasing temperature. This may cause an inverse dependence of the rate of atmospheric corrosion on temperature in some cases. Thus, Niklasson et al.<sup>34</sup> reported that the corrosion of lead exhibited a negative correlation with temperature in the presence of gaseous acetic acid. Esmaily et al.<sup>35</sup> showed that there was no clear correlation between temperature and the rate of atmospheric corrosion of Mg in the presence of NaCl.

Few studies report on the role of temperature in the atmospheric corrosion of Zn. Svensson et al.<sup>36</sup> reported an inverse temperature-dependence for the atmospheric corrosion of Zn in the presence of traces of  $\text{SO}_2$  in the range  $4$ – $20^\circ\text{C}$ , the highest corrosion rate being registered at the lowest temperature. According to Henriksen et al.,<sup>37</sup> Zn suffered corrosion in an outdoor environment (the northern parts of Norway) at temperatures well below  $0^\circ\text{C}$ . The authors<sup>37</sup> provided no details on the corrosion mechanism and corrosion products' composition at  $T < 0^\circ\text{C}$ . Thus, there is no systematic study of Zn corrosion at temperatures  $< 0^\circ\text{C}$ .

To fill this gap, the present paper investigates the NaCl-induced atmospheric corrosion behavior of Zn in the range  $-4$  to  $22^\circ\text{C}$  using a newly developed corrosion set-up that enables us to reliably examine the effect of temperature on the atmospheric corrosion of metals.<sup>38</sup> This study was done to advance the understanding of the Zn corrosion in real-world atmospheric environments, where the metal may experience significant temperature variations.

### Materials and Methods

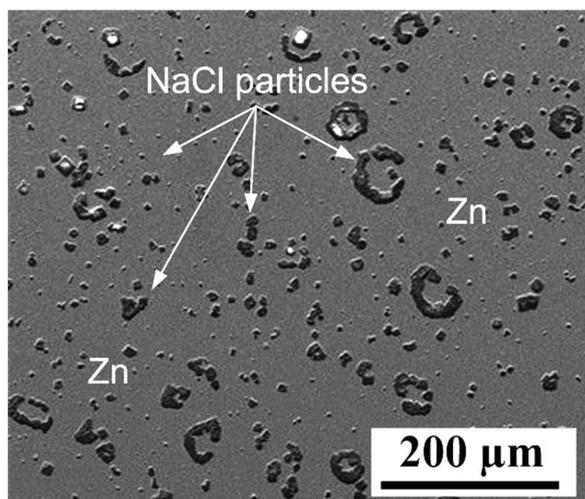
**Sample preparation.**—Electrolytic grade zinc (Zn 99.95% purity) was machined to obtain  $15 \times 15 \times 3 \text{ mm}^3$  coupons. Samples were ground using SiC grit papers (P1000 to P4000 mesh). Polishing was performed using diamond paste ( $0.25$ – $3 \mu\text{m}$ ). The amount of NaCl added to the surface, by spraying of a NaCl-containing solution of 80/20 ethanol/water,<sup>39</sup> was  $14$  or  $70 \mu\text{g}/\text{cm}^2$ . Care was taken to achieve an even distribution of NaCl on the sample surface (Fig. 1). The salt particles (in Fig. 1) ranged widely in size, from  $\sim 0.05$  to  $30 \mu\text{m}$ .

**Experimental set-up (Corrosion exposures).**—The exposure set-up is described elsewhere.<sup>39</sup> The gas flow in the chambers was  $1000 \text{ ml}/\text{min}$  corresponding to an average flow velocity of  $1 \text{ mm}/\text{s}$ . Relative

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**Figure 1.** A SEM image showing an even distribution of NaCl particles on the surface of Zn.

humidity (RH) was regulated to be  $95 \pm 0.3\%$ .  $\text{CO}_2$  concentration was  $400 \pm 20$  ppm. Exposures were performed at a wide range of temperatures ( $-4$  to  $22^\circ\text{C}$ ) with an overall accuracy of  $\pm 0.08$ – $0.12^\circ\text{C}$ .

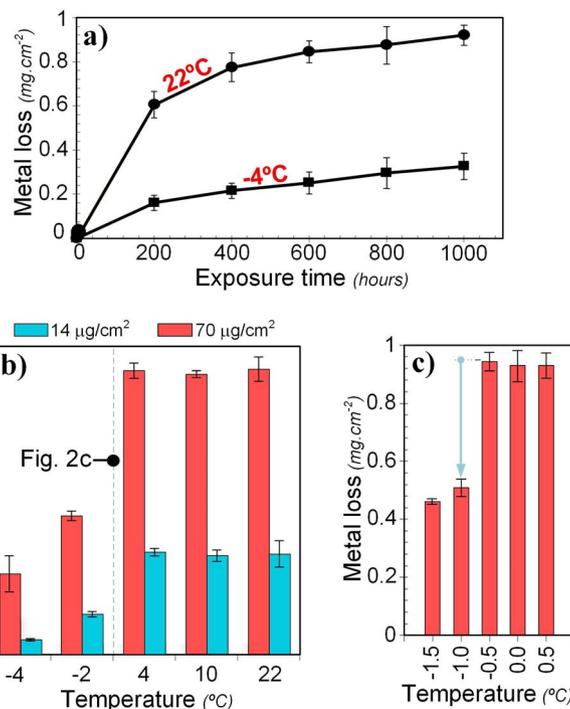
**Gravimetric measurement.**—Pickling was performed to determine the metal losses. Thus, water-soluble corrosion products were first removed by leaching in Milli-Q water. Afterwards, the samples were pickled several times in a saturated ammonium acetate ( $\text{NH}_4\text{C}_2\text{H}_3\text{O}_2$ ) solution (at  $22^\circ\text{C}$ ) until constant masses were registered. Self-corrosion during pickling was negligible.

**Methods of analysis.**—Corrosion products were studied using X-ray diffraction (XRD). XRD data were taken both by Bragg-Brentano (the normal mode) and grazing incidence (GIXD) angle geometries. The amount of water-soluble anions in the corrosion products was determined by the ion chromatography (IC) method using a Dionex 1000 equipped with an Ionpac AD4-SC Analytic Column. The eluent was  $1.8$  mM  $\text{Na}_2\text{CO}_3/1.7$  mM  $\text{NaHCO}_3$ .

Corrosion products were viewed using an FEI Quanta 200 environmental scanning electron microscopy (ESEM). Imaging was performed using secondary electrons (SE) and backscattered electrons (BSE). The instrument was equipped with Oxford Inca energy dispersive X-ray detector (EDX) system, with a beryllium window, that makes the quantification of carbon content in the corrosion products reliable.

To delineate the chemical composition of the thin oxide layer(s), we employed scanning transmission electron microscopy (STEM) and high-resolution Auger electron spectroscopy (HR-AES). The STEM analyses were performed in a Titan 80 instrument, equipped with an Oxford Inca EDX detector, operating at  $300$  kV. HR-AES depth profiling was performed in a site-specific manner (on an area of  $200 \times 200$  nm<sup>2</sup>) using a Physical Electronics Model 710 scanning auger nanoprobe (LS) equipped with a spherical sector analyzer. AES spectra were recorded in direct mode with a  $2$ – $5$  keV and  $1$  nA primary beam, a depth resolution of  $\sim 1.5$  nm, an elemental sensitivity down to  $0.1$  (in at. %) and a rather high lateral resolution of  $\sim 6$  nm.

We employed focused ion beam (FIB) milling method (using an FEI Versa 3D combined FIB/SEM workstation) to; (a) prepare cross sections through the corrosion products and metal substrate and also (b) to create site-specific in-situ lift-outs for the STEM analyses. This latter procedure<sup>39</sup> consists of several main steps; platinum (Pt) deposition with the aid of electrons and ions for protection, coarse ion milling (bulk-out), U-cut, lift out, mounting on a copper grid, thinning and finally a cleaning procedure.



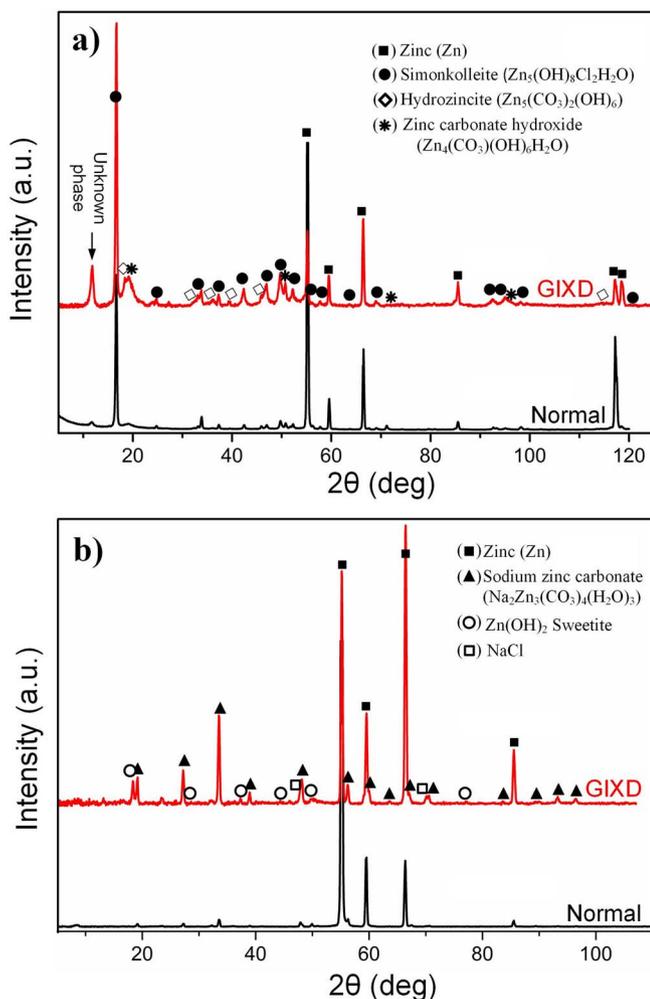
**Figure 2.** Corrosion of zinc as a function of time and temperature | (a) Metal loss at  $200\text{h} < t < 1000$  h at  $22$  and  $-4^\circ\text{C}$  (in the presence of  $70 \mu\text{g}/\text{cm}^2$  NaCl), (b) metal loss after  $1000$  h at  $-4$ ,  $-2$ ,  $4$ ,  $10$  and  $22^\circ\text{C}$  at two levels of NaCl, and (c) metal loss of Zn after  $1000$  h at  $0.5$ ,  $0.0$ ,  $-0.5$ ,  $-1.0$ , and  $-1.5$  V in the presence of  $70 \mu\text{g}/\text{cm}^2$  NaCl. All experiments were carried out in  $95\%$  RH air containing  $400$  ppm  $\text{CO}_2$ .

## Results

**Gravimetric measurements.**—Figure 2a presents metal losses of Zn in the presence of NaCl at  $22$  and  $-4^\circ\text{C}$  in  $95\%$  RH air containing  $400$  ppm  $\text{CO}_2$  as a function of exposure time. Initially, corrosion was considerably faster at  $22^\circ\text{C}$  compared to  $-4^\circ\text{C}$ . However, the rates of corrosion were almost the same during later stages ( $>600$  h). Figure 2b shows the metal loss after  $1000$  h exposure at  $-4$ ,  $-2$ ,  $4$ ,  $10$  and  $22^\circ\text{C}$  at two levels of added NaCl. The corrosion of the reference samples (exposed in the absence of salt) was negligible ( $<0.02$  mg/cm<sup>2</sup> after  $1000$  h). Finally, Fig. 2c shows metal loss after  $1000$  h exposure at  $-1.5$ ,  $-1.0$ ,  $-0.5$ ,  $0.0$  and  $0.5^\circ\text{C}$ .

Hence, corrosion rate is independent of temperature in the range  $-0.5$ – $22^\circ\text{C}$ . This is in accordance with Lindström et al.,<sup>21</sup> who studied the corrosion of Zn in the temperature range  $4$ – $40^\circ\text{C}$ . Also, the corrosion rates measured in the range  $-0.5$ – $22^\circ\text{C}$ , with metal losses after  $1000$  h of  $\sim 0.9$  and  $0.34$  mg/cm<sup>2</sup> ( $\sim 10.8$  and  $4.1$  μm/year) at  $70$  and  $14 \mu\text{g}/\text{cm}^2$  NaCl, respectively. In contrast, the present study shows that the rate of corrosion decreased rapidly below  $-0.5^\circ\text{C}$ , the mass losses registered at  $-1.0$ ,  $-1.5$  and  $-2.0^\circ\text{C}$  being about 50% of those measured in the range  $-0.5$ – $22^\circ\text{C}$ . Lowering the exposure temperature to  $-4^\circ\text{C}$  resulted in a further decrease in corrosion rate to about 25% of the level observed at  $-0.5^\circ\text{C}$  and higher. The same trend was observed for the mass gains (not shown). The temperature dependence of Zn corrosion did not depend on the amount of salt added.

**Corrosion product composition.**—XRD analysis was performed on some selective samples exposed at six different temperatures, three above and three below the “critical” temperature ( $-0.5^\circ\text{C}$ , see Fig. 2). Figure 3 shows two representative XRD patterns (both Bragg-Brentano and GIXD configurations) acquired from two specimens exposed  $-4^\circ\text{C}$  (below the critical T) and  $22^\circ\text{C}$  (above the critical T). The same crystalline corrosion products were identified after exposure at  $-0.5^\circ\text{C}$  and above. The diffraction pattern in Fig. 3a



**Figure 3.** XRD diffraction patterns of Zn after 1000 h in 95% RH air in the presence of  $70 \mu\text{g}/\text{cm}^2$  NaCl (a)  $22^\circ\text{C}$ , (b)  $-4^\circ\text{C}$ . Cr  $K\alpha$  radiation ( $\lambda = 2.29 \text{ \AA}$ ) was used.

was recorded after exposure at  $22^\circ\text{C}$  and showed that simonkolleite,  $(\text{Zn}_5(\text{OH})_8\text{Cl}_2 \cdot \text{H}_2\text{O})$ , was the dominant corrosion product. In addition, traces of hydrozincite,  $\text{Zn}_5(\text{CO}_3)_2(\text{OH})_6$ , and another zinc hydroxy carbonate,  $\text{Zn}_4(\text{CO}_3)(\text{OH})_6\text{H}_2\text{O}$  were detected. In some cases, the diffractograms contained an additional weak peak at  $2\theta = 12^\circ$  that could not be attributed to a known compound. Hydrozincite and  $\text{Zn}_4(\text{CO}_3)(\text{OH})_6\text{H}_2\text{O}$  were detected in the GIXD mode (Fig. 3a).

It was notable that none of the corrosion products identified by XRD at  $-0.5^\circ\text{C}$  and higher were detected after exposure at  $-1^\circ\text{C}$  and lower. Instead, the dominant crystalline corrosion product was sodium zinc carbonate hydrate  $\text{Na}_2\text{Zn}_3(\text{CO}_3)_4(\text{H}_2\text{O})_3$  together with small amounts of sweetite; (a tetragonal form of  $\text{Zn}(\text{OH})_2$ ). NaCl was identified by XRD after 1000 h at  $-2$  and  $-4^\circ\text{C}$ , but not at  $4$ – $22^\circ\text{C}$ , showing that, at low temperature, a significant fraction of the added NaCl remained unreacted after 1000 h.

The SEM micrographs in Fig. 4 show that exposure at  $22$  and  $-4^\circ\text{C}$  resulted in entirely different corrosion morphologies. In agreement with the gravimetric results (Fig. 2) the samples exposed at  $22^\circ\text{C}$  showed more evidence for corrosion than at  $-4^\circ\text{C}$ . Indeed, part of the metal surface appeared un-corroded after 1000 h exposure at  $-4^\circ\text{C}$ , see e.g., Fig. 4f. At  $22^\circ\text{C}$ , the corrosion products tended to form porous aggregates consisting of needlelike crystals covering the whole metal surface, while the corrosion products formed at  $-4^\circ\text{C}$  were denser.

In accordance with the XRD results, unreacted NaCl was detected by SEM/EDX after exposure at  $-4^\circ\text{C}$ , but not at higher temperatures, e.g.,  $22$ ,  $10$  and  $4^\circ\text{C}$ . The fraction of the surface covered by unreacted

salt (*fs*) was determined by SEM/EDX in a  $2 \text{ mm}^2$  area. The highest *fs* values were found at the lowest exposure temperature, image analysis showing that NaCl crystals covered 2.9% of the surface after 1000 h at  $-4^\circ\text{C}$ .

The fraction of water-soluble chloride on samples contaminated with  $70 \mu\text{g}/\text{cm}^2$  NaCl was determined by IC after 1000 h exposure at  $22$  and  $-4^\circ\text{C}$ . On the samples exposed at  $22^\circ\text{C}$  only 0.5% of the added chloride was leached by water, while the leachable fraction at  $-4^\circ\text{C}$  was 38%. Thus, nearly all the chloride added was incorporated in the corrosion products in insoluble form after exposure at  $22^\circ\text{C}$ . The XRD analysis of the corrosion products implies that much of the insoluble chloride was present in the form of simonkolleite. Conversely, the high fraction of water leachable chloride at  $-4^\circ\text{C}$  is in line with the absence of simonkolleite at that temperature.

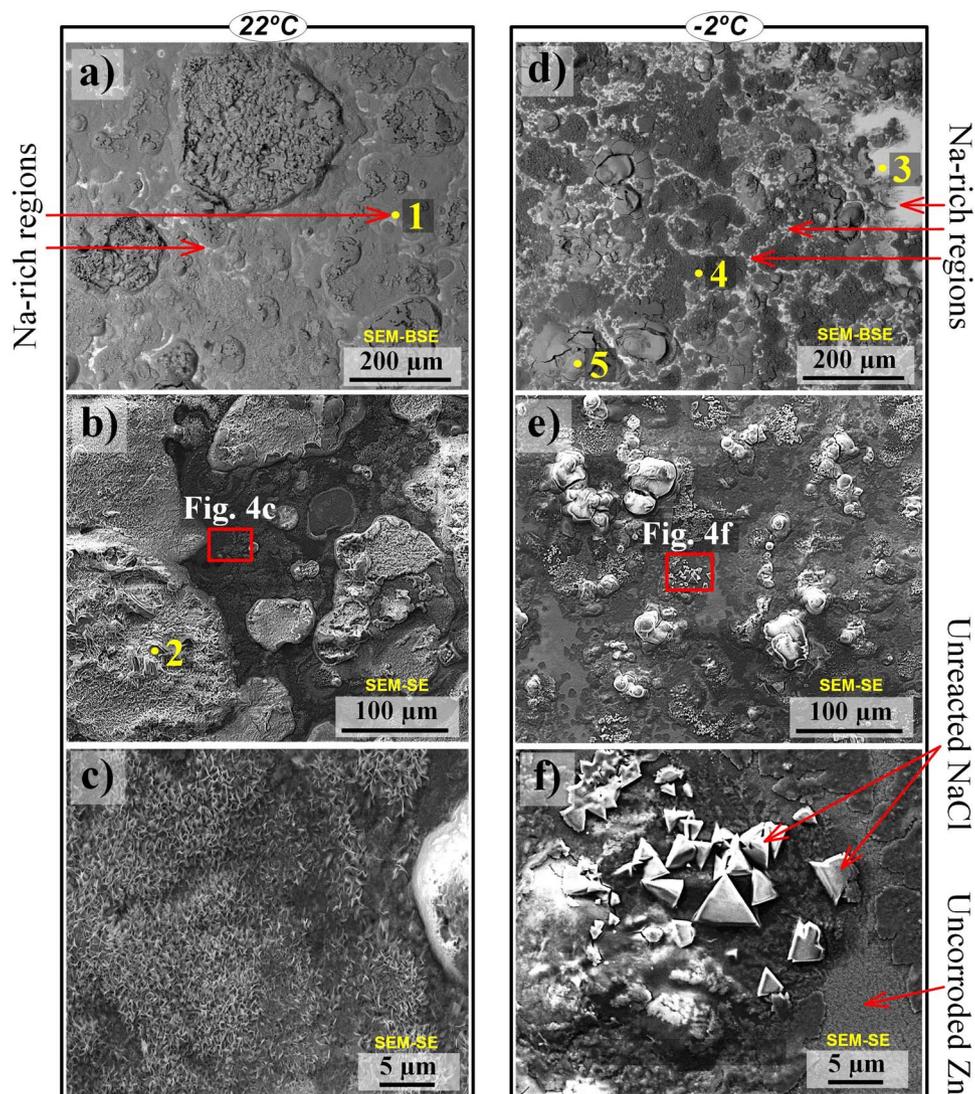
Table I lists SEM/EDX analyses of the points indicated in Figs. 4a, 4b and 4d. Points 1 and 4 are low in Zn and high in sodium, oxygen and carbon. Point 1 has a composition very close to  $\text{Na}_2\text{CO}_3$  and is thus identified as sodium carbonate. For position 4 the Na/C ratio is somewhat lower, suggesting the presence of both carbonate and hydrogen carbonate (e.g.,  $\text{Na}_3\text{CO}_3\text{HCO}_3 \cdot 2\text{H}_2\text{O}$ ). While sodium carbonate is expected to be present in hydrated form on the corroding sample i.e., as  $\text{Na}_2\text{CO}_3 \cdot 10\text{H}_2\text{O}$ , the water of hydration tends to be lost during dry storage and, especially, in the vacuum of the SEM. This explains why the analysis of point 1 corresponds to the anhydrous compound. Also, the lack of evidence for sodium carbonate and sodium carbonate hydrate by XRD is tentatively attributed to decomposition of the hydrated compound into poorly crystalline anhydrous (or amorphous) phases.

The composition at point 2 ( $22^\circ\text{C}$ ) is close to that expected for simonkolleite ( $\text{Zn}_5(\text{OH})_8\text{Cl}_2 \cdot \text{H}_2\text{O}$ ) which was the dominant crystalline corrosion product at  $22^\circ\text{C}$  according to XRD. Point 3 ( $-4^\circ\text{C}$ ), which appears as bright regions in Fig. 4d, exhibits an elemental ratio close to Na:Zn:Cl:O = 2:1:4:3 (Table I), corresponding to the compound  $\text{Na}_2\text{ZnCl}_4 \cdot 3\text{H}_2\text{O}$  which was not identified by XRD, however. Finally, point 5 ( $-4^\circ\text{C}$ ), and similar regions, had a composition close to sodium zinc carbonate, which was the main corrosion product at  $-2$  and  $-4^\circ\text{C}$  according to XRD. It may be noted that the presence of a Zn background signal and of additional carbon due to handling are likely to slightly offset the EDX analysis of the corrosion product from the “true” values.

Figure 5 shows SEM/STEM/EDX results of FIB-prepared specimens. In accordance with the identification of simonkolleite after exposure at  $22^\circ\text{C}$  by XRD and plan view SEM/EDX, Fig. 5a shows a corrosion product agglomeration formed at  $22^\circ\text{C}$  with a composition close to that of simonkolleite. Figure 5b shows a cross section of a sample after 1000 h at  $-4^\circ\text{C}$ , exhibiting a relatively small corrosion product agglomeration. The composition (Fig. 5b) corresponds to  $\text{Na}_2\text{Zn}_3(\text{CO}_3)_4 \cdot 3\text{H}_2\text{O}$ , which was detected both by XRD and plan view SEM/EDX (see Fig. 3, Table I). The corrosion product agglomeration is surrounded by regions dominated by Na, C and O showing a chemical composition similar to point 4 in Table I, corresponding to sodium carbonate and sodium hydrogen carbonate.

Figures 5c and 5d shows STEM micrographs of samples exposed at  $22$  and  $-4^\circ\text{C}$ , this time illustrating the relatively even corrosion product layers that in both cases covered much of the surface. Again, the morphology and composition of the corrosion product at the two temperatures is very different. At  $22^\circ\text{C}$ , the layered corrosion product had a thickness in the range  $0.8$  to  $1.5 \mu\text{m}$  (Fig. 5c). Its top part was porous and dominated by large blade-like crystallites. Based on the XRD analysis (Fig. 4) and the SEM/EDX cross section analysis (Fig. 5a), it is concluded that this layer consists of simonkolleite. Further down into the corrosion product there is an abrupt transition to a more compact region. A closer inspection revealed that the bottom “compact layer” had an internal structure and that a thin sub-layer could be identified closest to the Zn substrate which was even denser than the rest. The very dense, bottom part of the corrosion product is termed “barrier oxide” in Fig. 5c.

The compact middle and bottom layers contained only Zn and O, with a ratio close to Zn:O = 1, indicating zincite ( $\text{ZnO}$ ). To summarize,



**Figure 4.** SE and BSE SEM micrographs showing the corrosion morphology at 22°C (a, b and c) and  $-4^{\circ}\text{C}$  (d, e and f) after 1000 h exposure in the presence of 400 ppm  $\text{CO}_2$  and 95% RH and  $70 \mu\text{g}/\text{cm}^2$  NaCl. The chemical compositions of the points designated 1 to 5 are listed in Table I.

the corrosion product formed at  $22^{\circ}\text{C}$  consisted of a top simonkolleite layer, a middle ZnO layer and a bottom ZnO barrier layer. It may be noted that STEM/EDX revealed local Cl enrichments beneath the ZnO barrier layer, being associated with nano-sized pits in the metal substrate, see Fig. 5c.

Exposure at  $-4^{\circ}\text{C}$  produced a single, continuous, and very dense, 200–400 nm thick layer on the Zn surface. The layer shown in Fig. 5d is about 450 nm. The STEM/EDX analyses were consistent with  $\text{Na}_2\text{Zn}_3(\text{CO}_3)_4(\text{H}_2\text{O})_3$  which was detected both by XRD and

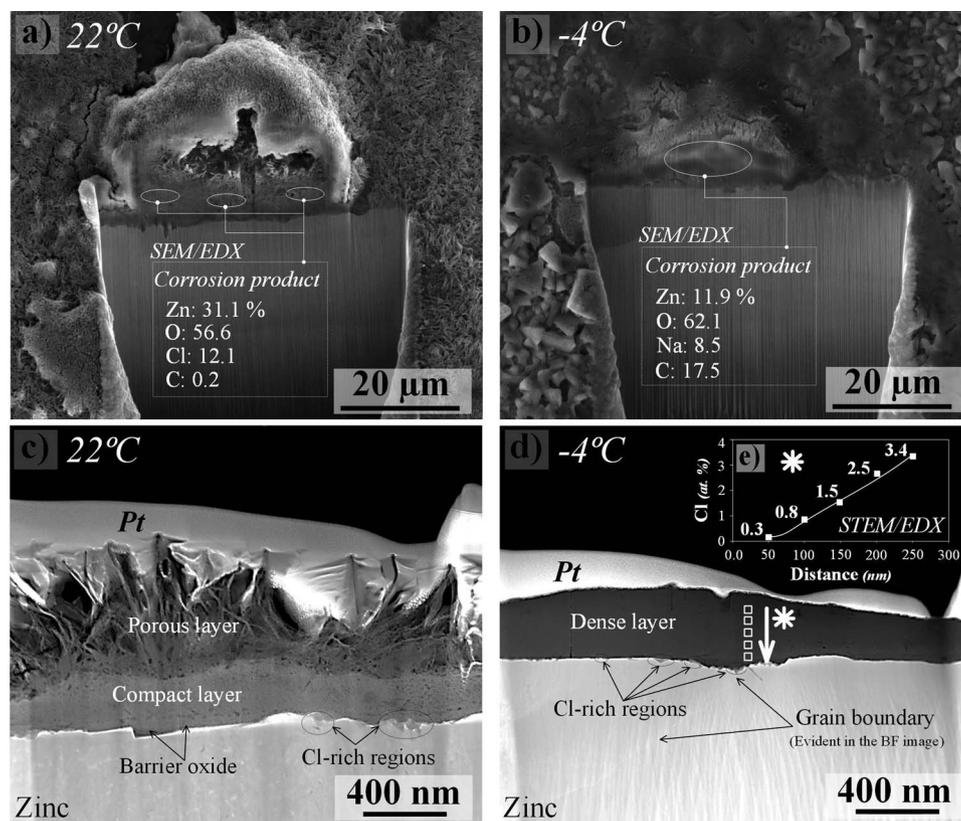
by SEM/EDX (see above). Interestingly, the layer contained significant amounts of chlorine, the Cl concentration increasing as the Zn surface was approached. The Cl gradient was almost linear and is shown in Fig. 5e. Similar to the  $22^{\circ}\text{C}$  sample, local Cl enrichments were detected at the alloy/corrosion product interface, associated with nanometer size pits in the metal substrate, see Fig. 5d.

These regions were very high in Cl (reaching 48–52 at. %) and Zn (28–32 at. %) with only small amounts of oxygen and no sodium, suggesting the presence of  $\text{ZnCl}_2 \cdot \text{H}_2\text{O}$ . Figure 5c reveals, tentatively,

**Table I.** Chemical composition (at.%) of the points indicated in Fig. 4. Note: The “matching compounds” were selected based on the comparing the elemental composition (ignoring H) and on the XRD analysis.

Point	Zn	C*	O	Cl	Na	Matching compounds
1	$1 \pm 0.2$	$15.1 \pm 1.8$	$52.5 \pm 1.2$	-	$31.5 \pm 0.5$	$\text{Na}_2\text{CO}_3$
2	$30.2 \pm 1.3$	$2.1 \pm 1.5$	$56.7 \pm 0.4$	$11 \pm 0.42$	-	$\text{Zn}_5(\text{OH})_8\text{Cl}_2\text{H}_2\text{O}$
3	$11.8 \pm 1.6$	$1.4 \pm 1.9$	$28.6 \pm 0.3$	$39.5 \pm 0.6$	$18.7 \pm 0.3$	$\text{Na}_2\text{ZnCl}_4 \cdot 3\text{H}_2\text{O}$
4	$2.5 \pm 0.7$	$15.7 \pm 2.1$	$56.2 \pm 0.3$	-	$25.6 \pm 1.5$	$\text{Na}_2\text{CO}_3$
5	$10.4 \pm 0.83$	$19 \pm 3.6$	$61.2 \pm 0.5$	$0.1 \pm 2.1$	$9.3 \pm 0.45$	$\text{NaCO}_3\text{HCO}_3 \cdot 2\text{H}_2\text{O}$ $\text{Na}_2\text{Zn}_3(\text{CO}_3)_4 \cdot 3\text{H}_2\text{O}$

\*The analysis for carbon was done using a SEM equipped with a beryllium window.



**Figure 5.** FIB/SEM/STEM/EDX investigation of Zn after corrosion at  $-4$  and  $22^{\circ}\text{C}$  | (a and b) SEM backscattered electron images of specimens exposed at; a)  $22^{\circ}\text{C}$ , b)  $-4^{\circ}\text{C}$ . The elemental compositions (by EDX) are in at.%, and (c - e) STEM micrographs and EDX analysis; (c) at  $22^{\circ}\text{C}$ , (d) at  $-4^{\circ}\text{C}$ , and (e) EDX analysis showing the Cl concentration in the corrosion product layer at  $-4^{\circ}\text{C}$  as a function of the distance to the surface of the corrosion product film. The samples were exposed for 1000 h at 95% RH in the presence of  $70\ \mu\text{g}/\text{cm}^2$  NaCl and 400 ppm  $\text{CO}_2$ .

preferential corrosion of a metal grain boundary. The grain boundary was also observed in bright field (BF) STEM micrographs of the same area (not shown).

In order to investigate the transition between the corrosion behavior of Zn at high and low temperature (Fig. 2), HR-AES compositional depth profiling was carried out on specimens exposed for 10 and 100 h at  $-0.5$  and  $-1^{\circ}\text{C}$ , see Fig. 6. In all cases (Figs. 6a–6e), the analysis reached to the metal substrate as evidenced by the Zn signal approaching 100 at.%. Due to surface contamination, the top ( $\sim 2$  nm) of the surface film was high in carbon on all samples.

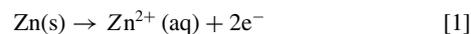
Figure 6 shows that the sudden transition between the faster high temperature corrosion at  $-0.5$  and the slower corrosion at  $-1.0^{\circ}\text{C}$  (compare Fig. 2) is accompanied by a complete change in the corrosion product composition. Thus, the results show that while ZnO is a major constituent of the surface film formed at  $-0.5^{\circ}\text{C}$  (Figs. 6a and 6b), ZnO is absent at  $-1.0^{\circ}\text{C}$  (Figs. 6c–6e). After 10 h at  $-0.5^{\circ}\text{C}$  (Fig. 6a), the film consisted of a 30 nm layer of ZnO.

After 100 h at  $-0.5^{\circ}\text{C}$  (Fig. 6b), the ZnO film had grown in thickness and has become covered by a very thin layer of zinc hydroxy carbonate. The presence of ZnO is reminiscent of the STEM micrograph in Fig. 5c. In contrast, the films formed at  $-1.0^{\circ}\text{C}$  (Figs. 6c–6e) are dominated by sodium zinc carbonate, similar to the film in the STEM micrograph in Fig. 5d. The profile in Figure 6d ( $-1^{\circ}\text{C}$ ) indicates the presence of a  $\text{Zn}(\text{OH})_2$  layer between the zinc substrate and the sodium zinc carbonate layer.

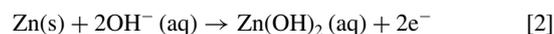
Table II presents all the corrosion products detected by XRD, SEMSTEM/EDX and HR-AES. Simonkollite, hydrozincite, Zn carbonate hydroxide, sodium carbonates, and ZnO were identified at temperatures at  $-0.5^{\circ}\text{C}$  and higher, while sodium zinc carbonate,  $\text{Na}_2\text{ZnCl}_4 \cdot 3\text{H}_2\text{O}$ , zinc hydroxide (sweetite), and sodium carbonates were identified at  $-1^{\circ}\text{C}$  and below.

## Discussion

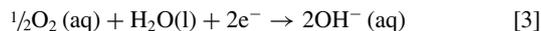
**Corrosion chemistry of Zn.**—When exposed to  $\text{O}_2$  or dry air at room temperature, Zn forms a passive film consisting of ZnO.<sup>27</sup> Under the experimental conditions (95% RH at  $-4^{\circ}\text{C} \leq T \leq 22^{\circ}\text{C}$ ), NaCl absorbs water and forms  $\text{NaCl}(\text{aq})$  droplets on the surface. The ZnO film tends to be attacked by the aqueous solution, resulting in electrochemical corrosion.<sup>26,40</sup> The anodic dissolution of Zn in acidic solution can be written:



In neutral and slightly alkaline solution the reaction is:



Water reduction occurs in oxygen-free solution,  $\text{O}_2$  is the main oxidant in aerated solution:<sup>26</sup>

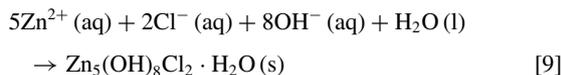


Zn dissolution causes chloride to accumulate in the anodic areas, the resulting  $\text{ZnCl}_2(\text{aq})$  anolyte being somewhat acidic. Conversely, the migration of  $\text{Na}^+$  ions to the cathodic areas result in the formation of a strongly alkaline  $\text{NaOH}(\text{aq})$  catholyte. Being amphoteric, ZnO dissolves as zincate ( $\text{Zn}(\text{OH})_3^-(\text{aq})$ ) at very high pH ( $>12$ ) and zinc is hence sensitive to corrosion at high pH, see Thomas et al.<sup>22,25</sup> However, under typical atmospheric corrosion conditions with very thin electrolyte layers and free access to  $\text{CO}_2$ , the very high pH values needed for zincate formation are not expected to occur (see below).

Zincite (ZnO) is an active substrate for the cathodic reduction of both  $\text{O}_2$  and  $\text{H}_2\text{O}$ ,<sup>24,41,42</sup> its cathodic activity being directly dependent on its semiconducting properties. In contrast, most other corrosion products reported to form on Zn in the ambient atmosphere are large band-gap insulators, and, therefore cannot be efficient cathodes.



Simonkolleite also forms by precipitation:



In accordance with the electrochemical nature of corrosion, the present study shows that Zn corrosion is localized at all temperatures investigated, see SEM images in Fig. 4. The positive correlation between the amount of salt added and the rate of corrosion (Fig. 2) is attributed to the amount of surface electrolyte formed, which is proportional to the amount of added NaCl.

**The effect of temperature.**—A NaCl(aq) solution in equilibrium with 95% RH at 22°C contains about 8.0% (wt%) NaCl.<sup>47,48</sup> Because the concentration of the NaCl(aq) electrolyte in equilibrium with 95% RH is almost independent of temperature in the experimental range,<sup>49</sup> the amount and composition of the NaCl(aq) solution is essentially the same at all temperatures studied. Also, the solution does not form ice in the temperature range studied.<sup>50</sup> Thus, the dependence of corrosion on temperature is not caused by differences in the amount or concentration of the electrolyte formed at the start of the experiment.

As mentioned in the introduction, there are few reports on the temperature dependence of the atmospheric corrosion of Zn. Lindström et al.<sup>9</sup> who investigated the NaCl-induced atmospheric corrosion of Zn at 4, 22 and 38°C reported no temperature dependence in the presence of CO<sub>2</sub>, but a strong positive correlation between corrosion rate and temperature in the absence of CO<sub>2</sub>. Svensson et al.<sup>24</sup> reported that the rate of SO<sub>2</sub>-induced Zn corrosion exhibited an inverse temperature-dependence which was attributed to a somewhat protective zinc hydroxy sulfate precipitate that nucleated at high temperature but not at low temperature.

The present results show that the rate of NaCl-induced corrosion of Zn in the presence of CO<sub>2</sub> is independent of temperature in the range −0.5–22°C. In contrast, corrosion rate drops suddenly when temperature is lowered to −1.0°C and below, see Fig. 2 and Fig. 4. The corrosion product composition is of special interest in the present study because the slower corrosion rate and change in corrosion morphology is accompanied by a drastic change in corrosion product composition (Table II). This suggests that there is a causal connection between corrosion rate and corrosion product composition. This hypothesis is explored in the following.

**Corrosion at “high” temperatures (−0.5°C ≤ T ≤ 22°C).**—The compounds identified after the exposures at high temperatures (Table II) have been previously reported as corrosion products on Zn in ambient air. Also, the analysis of the samples exposed at −0.5, 0.0, 0.5°C indicated essentially the same composition. As noted in the introduction, hydrozincite and simonkolleite are ubiquitous in the atmospheric corrosion of Zn, the latter often dominating in chloride-containing environments.<sup>4</sup> Falk et al.<sup>51</sup> identified Zn<sub>4</sub>(CO<sub>3</sub>)(OH)<sub>6</sub>H<sub>2</sub>O on Zn exposed to humid CO<sub>2</sub>-containing air and reported it to be metastable, being converted to hydrozincite with time. Zincite has been frequently reported as a corrosion product on Zn,<sup>24–26,52,53</sup> while sodium carbonate and sodium hydrogen carbonate have been reported to form on Zn exposed to humid air in the presence of NaCl.<sup>51,52</sup>

As noted above, ZnO is expected to play an important part in Zn corrosion, being an active cathode for O<sub>2</sub> reduction.<sup>24,25</sup> Indeed, the present study shows that a layer of zincite forms on the Zn surface at −0.5°C and higher. For example, the cross section SEM/EDX (Fig. 5a) and STEM/EDX (Fig. 5c) (22°C, 1000 h) images show a layered corrosion product where the upper part consist of agglomerated simonkolleite crystallites. The lower strata in the corrosion product consist of zincite, forming a very dense, 30–50 nm, barrier-like layer in contact with the metal and a somewhat more porous layer immediately below the simonkolleite. Thus, at 4, 10 and 22°C, a large part of the corroding Zn surface is covered by a duplex ZnO layer. Notably, the STEM/EDX analysis of a cross section revealed traces of chloride in the “barrier” ZnO layer and chloride-rich corrosion pits in the Zn substrate, see Fig. 5c. Also, the HR-AES compositional depth profiles

in Figs. 6a and 6b (−0.5°C, 10 h, 100 h) show that a ZnO layer is rapidly established on the Zn substrate. Interestingly, the AES analysis shows a gradual buildup of zinc hydroxy carbonate layer on top of the ZnO layer which can be observed after 100 h at −0.5°C (Fig. 6b). That layer has a composition similar to that of the metastable Zn<sub>4</sub>(CO<sub>3</sub>)(OH)<sub>6</sub>·H<sub>2</sub>O and, probably, formed according to Reaction 7. The layer does contain some chloride and it is hypothesized that it may be converted to simonkolleite with time.

The corrosion morphology observed after 1000 h at 4, 10 and 22°C is reminiscent of that reported by McDonald et al.<sup>54</sup> who observed the formation of a duplex ZnO layer under anodic dissolution of Zn in alkaline solution. The duplex film consisted of a few nm thick, dense inner “barrier” ZnO layer, which, was proposed to have formed by a solid state reaction, and an outer, porous, ZnO layer precipitated from solution (see Reaction 5). The corrosion morphology is even more similar to that reported by Thomas et al.<sup>25</sup> after 6h exposure of Zn to a drop of seawater in air. They observed an outer macro-porous layer, covering a less porous ZnO-containing middle layer and an about 50 nm thick, dense, ZnO bottom layer. Also, they observed chloride-induced pitting below the ZnO layers. Thomas et al.<sup>24–26</sup> present a corrosion scenario postulating that the ZnO layers contain pores that penetrate to the metal, metal dissolution in the pore being coupled to cathodic reduction of oxygen and water on the pore walls and on the metal.

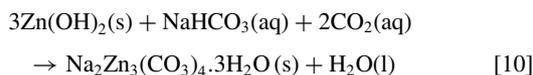
In accordance with the work of Thomas et al.,<sup>24,25</sup> the corrosion morphology observed at 4, 10 and 22°C is interpreted in terms of an electrochemical corrosion process in an aqueous electrolyte. Thus, although the bottom ZnO layer is seemingly dense, both ZnO sub-layers are considered to be permeable to the chloride-containing electrolyte. This implies that any “barrier” ZnO layer which may have been present at the start of the experiment is now penetrated by the aqueous electrolyte. O<sub>2</sub> reduction (Reaction 3) occurs in the outer, porous, part of the ZnO layer (O<sub>2</sub> reduction at the ZnO/simonkolleite interface is not likely because simonkolleite is not compatible with the alkaline conditions in the catholyte). The cathodic process is coupled to the anodic dissolution of Zn (Reactions 1 and/or 2 below the ZnO layer. This is consistent with the growth of a ZnO layer by precipitation (Reactions 4 and 5. The reduction of O<sub>2</sub> within the ZnO layer requires the simonkolleite layer to be permeable to O<sub>2</sub> transport, in agreement with its observed porosity. Significant water reduction in the pits, as suggested by Zhang<sup>55</sup> would tend to re-passivate the Zn surface and is therefore deemed less likely. Thus, the relatively fast corrosion in the range −0.5–22°C is related to the formation of a poorly protective zincite layer which acts as catalyst for cathodic O<sub>2</sub> reduction. Accordingly, it has been reported that ZnO layers formed at pH < 12 tend not to passivate the metal in the presence of chloride.<sup>56</sup>

The present finding that the rate of corrosion of Zn is independent of temperature when exposed at >−0.5°C, in the presence CO<sub>2</sub>, is in accordance with Lindström et al.<sup>16</sup> In contrast, the same authors<sup>16</sup> reported a strong positive temperature dependence of corrosion in the absence of CO<sub>2</sub>, suggesting that the lack of temperature dependence is connected to CO<sub>2</sub>. Also, Falk et al.<sup>51</sup> reported that CO<sub>2</sub> inhibits Zn corrosion. In agreement with others,<sup>9,20</sup> it is considered that the observed trend is connected to the inhibitive effect of CO<sub>2</sub>, which, in turn, depends on the formation of carbonic acid. It may be noted that while the solubility of CO<sub>2</sub> increases with decreasing temperature, the conversion of CO<sub>2</sub>(aq) to carbonic acid is a slow, thermally activated process.<sup>39,57</sup> It is hypothesized that the two antagonistic temperature dependencies cancel out, explaining the lack of temperature dependence of corrosion in the range −0.5–22°C.

**Corrosion at “low” temperatures (−4°C ≤ T < −0.5°C).**—The corrosion products formed at low temperatures were very different from those generated at “high” temperature (Table II), sodium carbonate being the only product occurring regardless of temperature. The dominant corrosion product was sodium zinc carbonate, Na<sub>2</sub>Zn<sub>3</sub>(CO<sub>3</sub>)<sub>4</sub>·3H<sub>2</sub>O (XRD results in Fig. 3, STEM in Fig. 5d, and AES profiles in Figs. 6c–6e). This compound was previously detected by Ortiz et al.<sup>58</sup> on Zn-Mn coated steel subjected to salt spray

testing. In addition, Prosek et al.<sup>59</sup> suggested that it formed on Zn-plated steel exposed to humid air/NaCl. In both cases, the compound was reported to form at ambient temperature or higher. The present study apparently is the first to positively identify sodium zinc carbonate as the *principal* corrosion product of Zn.

Sweetite, a tetragonal form of Zn(OH)<sub>2</sub>, was also only detected after the low temperature exposures. While wulfingite ( $\epsilon$ -Zn(OH)<sub>2</sub>) has been reported as a corrosion product previously,<sup>60</sup> the present study appears to be the first to identify sweetite as a corrosion product. As noted above, crystalline zinc hydroxides are reported to be more soluble than ZnO.<sup>55,61</sup> Hence, the formation of sweetite is attributed to kinetics and not to equilibrium thermodynamics. Accordingly, it is proposed that the nucleation of sweetite is faster than zincite at low temperature. In addition to the identification of sweetite by XRD, the presence of zinc hydroxide at low temperature is also evidenced by the AES analysis in Fig. 6d showing a Zn(OH)<sub>2</sub> layer which is sandwiched between Na<sub>2</sub>Zn<sub>3</sub>(CO<sub>3</sub>)<sub>4</sub> · 3H<sub>2</sub>O and the Zn substrate. The close association of the two compounds suggests that sodium zinc carbonate is formed by the reaction of zinc hydroxide with the surface electrolyte:



The third “low” temperature corrosion product detected was Na<sub>2</sub>ZnCl<sub>4</sub> · 3H<sub>2</sub>O, which was identified by STEM/EDX. Prosek et al.<sup>41</sup> tentatively identified it as one of several corrosion products on a ZnAlSi alloy exposed to humid air and NaCl at 20°C. Na<sub>2</sub>ZnCl<sub>4</sub> · 3H<sub>2</sub>O is highly soluble in water and needs high concentrations of NaCl(aq) in order to precipitate from solution.<sup>42</sup> This is in accordance with the identification of unreacted NaCl(aq) after the exposure. Also, Na<sub>2</sub>ZnCl<sub>4</sub> · 3H<sub>2</sub>O is hydrolyzed in neutral or alkaline conditions, revealing that slightly acidic conditions prevail on parts of the corroding surface.

To summarize, the corrosion products generated by the relatively rapid corrosion at “high” temperatures were dominated by simonkolleite and ZnO together with small amounts of zinc hydroxy carbonates, while the slower corrosion at “low” temperatures was associated with a corrosion product where simonkolleite, ZnO, and crystalline zinc hydroxy carbonates were absent. Instead, sodium zinc carbonate (Na<sub>2</sub>Zn<sub>3</sub>(CO<sub>3</sub>)<sub>4</sub>(H<sub>2</sub>O)<sub>3</sub>) dominated along with smaller amounts of sweetite (Zn(OH)<sub>2</sub>) and Na<sub>2</sub>ZnCl<sub>4</sub> · 3H<sub>2</sub>O.

Accordingly, the STEM image after “low” temperature exposure (Fig. 5d) shows a thick sodium zinc carbonate layer on the surface. In addition, the AES analysis (Fig. 6D) reveals the presence of a thin zinc hydroxide layer between zinc and the sodium zinc carbonate layer. Similar to the duplex ZnO layer formed at “high” temperatures, the Na<sub>2</sub>Zn<sub>3</sub>(CO<sub>3</sub>)<sub>4</sub>(H<sub>2</sub>O)<sub>3</sub>/Zn(OH)<sub>2</sub> layer seems dense but is apparently permeable to chloride ions, as evidenced by the linear chlorine gradient through it and by the presence of chlorine-enriched corrosion pits in the metal. The observations strongly suggest that corrosion is electrochemical also in this case.

Because both Na<sub>2</sub>Zn<sub>3</sub>(CO<sub>3</sub>)<sub>4</sub>(H<sub>2</sub>O)<sub>3</sub> and Zn(OH)<sub>2</sub> are large band-gap insulators, the layer covering the Zn surface cannot be cathodically active. Hence, the cathode must be situated at a distance from the anodic sites, presumably in the vicinity of the sodium carbonate precipitates observed in plan-view (Point 4 in Fig. 4d). While zincite was not observed, the cathodic activity is suggested to be associated with ZnO also in this case, e.g., to remnants of the air-formed ZnO surface film present at the start of the exposure. The presence of unreacted NaCl after the exposure shows that there is ample electrolyte on the surface to support such a process.

**Comparing the “low” and “high” temperature corrosion modes.**—The discussion above shows that the mechanism of Zn corrosion at low temperature (−4°C ≤ T ≤ −1°C) is fundamentally different from corrosion at higher temperature (−0.5°C ≤ T ≤ 22°C). This difference is attributed to the occurrence of ZnO. As mentioned above, the zinc hydroxides are more soluble and thus less stable than

ZnO, according to equilibrium thermodynamics. Thus, the replacement of ZnO by zinc hydroxide (sweetite) at low temperature must be explained by kinetics, in this case the rate of nucleation of two solids. Thus, the lack of direct evidence for ZnO and the identification of sweetite (Zn(OH)<sub>2</sub>) at low temperature implies that, even though ZnO is thermodynamically stable on the corroding surface at all temperatures studied, zincite precipitation is inhibited at −1°C and below. The temperature dependence of zincite precipitation is not unexpected, considering that the nucleation of a phase is always thermally activated.

Therefore, at “low” temperature, zincite is replaced by Zn(OH)<sub>2</sub>(s) which is electronically insulating and therefore cannot play the role of cathode. The AES analysis of the corrosion product layer formed after 100 h at low temperature (Fig. 6d) shows a thin zinc hydroxide film sandwiched between the metal and the sodium zinc carbonate layer.

We believe that the zinc hydroxide layer formed initially and that the sodium zinc carbonate formed from it (see Reaction 10). In this way a situation arises where the zinc anode becomes spatially separated from the cathode by a layer of corrosion products, which is cathodically inactive. It may be noted that while the duplex zincite layer formed at higher temperatures (Fig. 5c) and the sodium zinc carbonate/Zn(OH)<sub>2</sub> layer formed at low temperature (Figs. 5d and 6d) are both apparently permeable to chloride ions and water, allowing the anodic dissolution of the Zn substrate, the two layers differ a lot in properties. Importantly, zincite is an active cathode for O<sub>2</sub> reduction, while both zinc hydroxide and sodium zinc carbonate are electronic insulators and cannot act as cathodes. Consequently, in the low temperature mode of corrosion, the anodic dissolution of zinc below the electronically insulating layer is presumably coupled to cathodic O<sub>2</sub> reduction on parts of the surface where the original ZnO film remains. In contrast, the high temperature form of corrosion is characterized by the close proximity of anodic and cathodic surfaces, the poorly protective zincite layer acting as substrate for cathodic O<sub>2</sub> reduction.

This study shows that the peculiar temperature dependence of the atmospheric corrosion of Zn is not due to some activated process (e.g., charge transfer or ionic conduction) limiting the rate of a single corrosion process. Instead, it is due to a change in the mechanism of corrosion which is temperature related.

The present results, showing that the “low” temperature corrosion mode is significantly slower than the “high” temperature mode, are notable considering that the NaCl(aq) electrolyte was consumed by formation of simonkolleite and sodium carbonate at “high” temperature while it remained throughout the exposure at “low” temperature. Tentatively, the slower corrosion at low temperature is attributed to the greater separation of anode and cathode in the electrochemical corrosion cell.

The lack of temperature-dependence of corrosion in the high temperature range was discussed above. The low-temperature corrosion mode was observed in several experiments (−1, −1.5, −2, −4°C, 14 and 70 μg/cm<sup>2</sup> of NaCl). While the small range of temperatures does not allow us to draw definite conclusions regarding the temperature-dependence of the low temperature corrosion mode, the observed positive temperature dependence of corrosion at low temperature suggests that corrosion rate in this regime is limited by one or more activated processes.

In summary, the peculiar temperature dependence of the rate of NaCl-induced atmospheric corrosion of Zn is attributed to a change in corrosion mechanism that occurs between −0.5 and −1°C. The change in corrosion mechanism, in turn, is caused by the replacement of ZnO by Zn(OH)<sub>2</sub> at low temperature. The present findings may prove useful for interpreting the atmospheric corrosion of Zn and Zn-plated steel in automotive applications where the materials are exposed to NaCl at low temperature and high humidity.

All in all, addressing the properties of the corrosion product layer, i.e., sodium zinc carbonate (Na<sub>2</sub>Zn<sub>3</sub>(CO<sub>3</sub>)<sub>4</sub> · 3H<sub>2</sub>O/Zn(OH)<sub>2</sub>) and the characteristic of the relatively slow “low” temperature corrosion mode may open up an opportunity to improve the atmospheric corrosion behavior of Zn. Therefore, one exciting future research track would be

to investigate whether the corrosion behavior of Zn may be improved via promoting the formation of such layers. This would involve investigating how such layers can be formed in an appreciable amount at room temperature and higher, enabling their application under “real” service conditions.

### Conclusions

We studied the NaCl-induced atmospheric corrosion of Zn at different temperatures in the range  $-4$  to  $22^\circ\text{C}$ . Measurements of the corrosion rate and analysis of the composition/morphology of corrosion products formed allowed us to draw the following main conclusions:

- While the NaCl-induced atmospheric corrosion of Zn was independent of temperature in the range  $-0.5$ – $22^\circ\text{C}$ , corrosion rate dropped significantly at  $-1.0$ ,  $-1.5$ ,  $-2$  and especially, at  $-4^\circ\text{C}$ .
- The peculiar temperature dependence of the rate of NaCl-induced atmospheric corrosion of zinc is attributed to a change in corrosion mechanism that occurs between  $-1.0$  and  $-0.5^\circ\text{C}$ .
- The “high” temperature mode of corrosion (at  $-0.5^\circ\text{C}$  and higher) is characterized by the formation of a poorly protective ZnO layer on the surface. Cathodic  $\text{O}_2$  reduction occurs in pores in the ZnO layer while anodic dissolution of Zn occurs below the ZnO layer. In this corrosion mode the principal corrosion products were hydrozincite, simonkolleite and ZnO.
- At  $-1.0^\circ\text{C}$  and below, ZnO was replaced by  $\text{Zn}(\text{OH})_2$ . Corrosion resulted in the zinc surface being covered by a sodium zinc carbonate ( $\text{Na}_2\text{Zn}_3(\text{CO}_3)_4 \cdot 3\text{H}_2\text{O}$ )/ $\text{Zn}(\text{OH})_2$  layer. While this layer is permeable to chloride ions and water, it is electronically insulating. This results in a separation of the anode below the layer and the cathode on other parts of the metal surface. The main corrosion products in the low temperature corrosion mode were  $\text{Na}_2\text{Zn}_3(\text{CO}_3)_4 \cdot 3\text{H}_2\text{O}$ ,  $\text{Zn}(\text{OH})_2$  (sweetite) and  $\text{Na}_2\text{ZnCl}_4 \cdot 3\text{H}_2\text{O}$ . This is the first identification of sweetite as a corrosion product.
- While the rate of the high temperature mode of corrosion was temperature independent, the low temperature corrosion mode showed a positive correlation with temperature.

### Acknowledgment

We would like to deeply thank Professor Polina Volovitch (Chimie ParisTech, France) and Dr. Mats Ström (Volvo Car Cooperation) for helpful discussion. Also, we appreciate the Swedish Foundation for Strategic Research (SSF) (grant number: RMA08-0138) and the Swedish Research Council (Vr) (grant number: 2015–04977) for funding this research.

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