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# Linking the effect of reservoir injectivity and $\mathrm{CO}_{2}$ transport logistics in the Nordic Region 

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#### Abstract

We compare the cost for $\mathrm{CO}_{2}$-transport by ship with cost for pipeline transport in the Nordic region as a function of transport volume and distance. We also calculate the pipeline volumetric break-even point yielding the minimum $\mathrm{CO}_{2}$ volume required from a specific site for pipeline to become the less costly transport option and finally, we investigate the effect injectivity may have on the choice of reservoir and transport mode. Most stationary $\mathrm{CO}_{2}$-emissions in the Nordic region originate from emission intensive industries such as steel, cement and chemical plants and refineries. Typically, their emissions are modest (less than 1 Mt per year) compared to large coal fired power plants, while distances to potential storage sites are considerable, often 300 km or more. Hence, build-up of clusters of emission sources and $\mathrm{CO}_{2}$-volumes is likely to take time and be costly. At the same time, many of the emission sources, both fossil based and biogenic, are located along the coast line. The results imply that due to modest $\mathrm{CO}_{2}-$ volumes and relatively long transport distances $\mathrm{CO}_{2}$ transport by ship is the least costly transportation option for most of the sources individually as well as for most of the potential cluster combinations during ramp-up of the CCS transport and storage infrastructure. It is furthermore shown that cost of ship transport increases modestly with increasing transport distance which, in combination with poor injectivity in reservoirs in the Baltic Sea, indicate that it may be less costly to transport the $\mathrm{CO}_{2}$ captured from Finnish and Swedish sources located along the Baltic Sea a further $800-1300 \mathrm{~km}$ to the west by ship for storage in aquifers with higher injectivity in the Skagerrak region or in the North Sea.


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## 1. Introduction

In order to limit the global temperature increase to $2^{\circ} \mathrm{C}$ the EU has suggested that developed countries should reduce their GHG emissions by 80 to $95 \%$ relative to 1990 emissions by 2050 [1]. According to IEA [2] all Nordic countries ${ }^{\dagger}$ have long-term climate- and energy-related targets and visions that are ambitious and often surpass EU strategies, but with differences between the countries. Such targets have been even more relevant today, considering the recent agreement in the COP21 meeting in Paris, where it was expressed that global warming should be limited to well below $2^{\circ} \mathrm{C}$ [3].

A substantial part of the electricity generated in the Nordic region is generated by hydro, biomass, wind and nuclear energy, thus yielding low overall $\mathrm{CO}_{2}$-emissions. Also, owners of large coal power plants in Denmark and Finland have announced firm plans to switch to biomass based electricity generation (see for instance [4, 5]). Hence, most of the stationary fossil based emissions in the Nordic region will, in the future, probably arise from the energy intensive industry, such as from the cement and steel sectors and from refineries and chemical plants. Common for these industries, is that CCS has been shown to be a key mitigation measure in a portfolio of measures required to limit the global temperature increase to $2^{\circ} \mathrm{C}[6,7]$. IEA [2] has for instance suggested that $50 \%$ of cement plants and at least $30 \%$ of iron and steel and chemical industries in the Nordic countries should be equipped with CCS in 2050.

There are almost 300 emission sources in the Nordic region that emit $100 \mathrm{kt} \mathrm{of} \mathrm{CO}_{2}$ or more (biogenic or fossil) and it can only be speculated if and when the various sites will install capture, i.e. $\mathrm{CO}_{2}$ volume and potential clusters and transportation systems can potentially evolve into any configuration over time. At the same time cost for pipeline transport is sensitive to the volume being transported and most $\mathrm{CO}_{2}$-sources located in the Nordic region are located along the coast while storage sites are located offshore making also ship transport a potentially feasible transport option. Furthermore, the option of ship transport appears relevant since most emission source in the Nordic countries have relatively low emissions (compared to large coal fired power plants) and long distances to potential storage sites (most sources emit between $100 \mathrm{kt} \mathrm{up} \mathrm{to} 1 \mathrm{Mt} \mathrm{CO}_{2}$ per year and are located 300 km and more from a potential storage site). Ship transport is also particularly interesting during ramp-up of a $\mathrm{CO}_{2}$ transport system due to its flexibility allowing addition of multiple capture sites and storage sites over time. Thus, capacity can be added to the system (transport and/or storage) only if and when the need for increased capacity materializes and it is also possible to switch capture and/or storage sites altogether.

At the same time, preliminary analysis of potential storage sites in the Baltic Sea indicate poor storage and injection capacity $[8,9,10]$. This implies that the $\mathrm{CO}_{2}$ from sources located along the Swedish east coast and the Finnish west coast, may have to be transported between 800 and 1300 km further to the west for storage in reservoirs in the Skagerrak region or in the North Sea. Hence, the potential effect this may have on transport structure and its cost needs to be analyzed in detail.

The main aim of this paper is to conduct a comprehensive assessment of potential $\mathrm{CO}_{2}$ transport options in the Nordic region taking into consideration both individual emission sites and potential storage reservoirs. The work presented in this paper is based on work done partly in the NORDICCS project [11]. The paper is organized as follows; Section 2 explains the methodology applied in this work while results are given in Section 3. Section 4 discusses the results while main conclusions are given in Section 5.

## 2. Methodology

In this paper costs of different $\mathrm{CO}_{2}$ transportation options are analyzed by 1) comparing the cost for ship and pipeline transport as a function of volume and distance and by 2 ) calculating the pipeline volumetric break-even point, i.e. the volume required from any specific site for pipeline to be the least cost transport alternative in comparison with ship transport. We also analyze the effect injectivity may have on the choice of reservoir and thus also on the transport system.

[^1]In Section 3.1 we compare the cost of $\mathrm{CO}_{2}$ transport by pipeline and ship for increasing volumes and distances. Specific cost for transport by pipeline and by ship are compared for transport distances between 50 and 800 km and for transport volumes between 0.5 and 5.0 Million tonnes per annum (Mtpa).

In Section 3.2 it is assumed that a transport hub may be developed at eight selected sites in the Nordic region. For each of the eight selected transport hubs it is calculated for what volumes (and the corresponding cost) offshore pipeline transport becomes less costly than ship transport to three selected storage sites, i.e. the so-called pipeline volumetric break-even point. Thus, the least costly transport mode from the selected hubs is defined for any combination of clusters transporting $\mathrm{CO}_{2}$ to the selected storage site. The selected transport hubs represent a relevant geographical distribution of large-scale stationary $\mathrm{CO}_{2}$ emission sources in the Nordic region. The selected storage sites used for the transport cost calculations represent the reservoir for which we have the best data available in each of the three offshore regions that are relevant for the Nordic region, i.e. Faludden with respect to storage in the Baltic Sea, Gassum with respect to storage in the Skagerrak region and Utsira with respect to storage in the North Sea.

In Section 3.3 it is analyzed how the reservoir injectivity may influence the choice of reservoir. The latter is particularly important in the Nordic region if the assumed storage sites in the Baltic Sea turns out to have modest or poor storage and injection capacity as has been indicated in recent reports [8, 10].

Figure 1 shows all emission sources in the Nordic region with 2010 emissions of at least 100 ktonnes as well as the eight selected sites of large individual $\mathrm{CO}_{2}$ emission sources where it has been assumed that regional $\mathrm{CO}_{2}$-hubs may develop (yellow circles with corresponding case number). Also shown is the three selected storage sites (light yellow ellipses). It should be noted that the size and shape of the three storage sites are illustrative only.


Figure 1: Emission sources in the Nordic region with 2010 emissions of at least 100 ktonnes (green), eight selected sites for development of clusters (yellow circles with case number) plus relevant storage sites (light yellow). From [11].

Basic assumptions and input parameters to all transport systems are (unless otherwise specified):
a) All cost calculations (pipeline and ship) starts at 70 bar and $20^{\circ} \mathrm{C}$ at the $\mathrm{CO}_{2}$-hub and ends at the storage site at a pressure of 70 bar and $0-20^{\circ} \mathrm{C}$ at sea level. Maximum pressure in offshore pipelines has been set to 70 bar plus pressure drop depending on distance to the storage site. $\mathrm{A}_{2} \mathrm{CO}_{2}$ purity of $99 \%$ is assumed.
b) Transport distances have been measured in a Geographical Information System to which a "terrain factor" of $10 \%$ was added to the offshore distance for both ship and pipeline.
c) Ship sizes are optimized for each transport system but with max size set to $40000 \mathrm{~m}^{3}$, transport at 7 bar and minus $50^{\circ} \mathrm{C}$, speed 12 knots, 16 hours for loading and 54 hours to unload the $\mathrm{CO}_{2}$. Cost for
liquefaction, intermediate storage (on barges with volumes corresponding to the size of ships required for the transport), port fees and loading/unloading have been included.
d) Cost has also been included for pumping (from 7 to 70 bars) and heating of the $\mathrm{CO}_{2}$ from minus 50 up to zero degrees Celsius at the storage site through utilization of waste heat from the ship and use of sea water.
e) All transport systems include cost at the storage site, namely; cost of the required number of subsea templates with well heads, distribution lines between templates and umbilicals.
f) Cost has been calculated using the net present value method, discount rate has been set to $8 \%$ over 25 years (2 years construction, 23 years of operation). All initial cost data have been based on [12, 13] but the initial data has been updated and modified based on industrial experience and discussions with the industry. Cost data has been adjusted to 2014 Years cost level based on Eurostat's Consumer Price Index.

For the plants situated around Bothnia Bay (see Figure 1), the offshore transport distance to relevant storage sites is $1,000 \mathrm{~km}$ or more. For pipeline transport this will lead to very large pipelines as the volume increases, in particular if there are no booster stations along the transport route. In this work it was decided to set maximum offshore pipeline diameter to 48 inches. If the diameter exceeded 48 inches two equally large pipeline strings was assumed to be constructed.

## 3. Results

### 3.1. Comparing the cost of pipeline and ship transport

Figure 2 compares specific cost for transport by pipeline and by ship for transport distances between 50 and 800 km and for transport volumes between 0.5 and 5.0 Mtpa . Cost for ship transport is shown as solid lines while pipeline transport carrying the same volume is indicated by dashed lines. The break-even points where pipeline transport becomes more costly than ship transport are marked by circles and the corresponding distance is quoted.


Figure 2: Comparison of pipeline and ship transport cost (in $€$ per ton $\mathrm{CO}_{2}$ ) as function of volume and distance.

From Figure 2 it can be seen that the break-even distance where ship transport becomes less costly than pipeline transport increases as the transport volume increases, from roughly 65 km for transport of 0.5 Mtpa to more than 700 km for transport of 5 Mtpa . Figure 2 also implies that;

1) Ship transport cost increases modestly with increasing distance
2) Out of a total of fifty-five sources located along the coast and with an individual annual capture volume of 0.5 Mt or more (assuming $85 \%$ capture ratio on 2010 emissions) we can derive that:
a. Twenty-two of these sources have an individual capture potential between 0.5 and 1.0 Mtpa while at the same time their distance to the nearest storage site exceeds 165 km . Thus Figure 2 indicates that for these sources ship transport will be less costly than pipeline transport.
b. Another twenty-two of the fifty-five sources have a capture potential between 1 and 2 Mtpa and an individual transport distance to the nearest storage site exceeding 275 km . Thus Figure 2 indicates that also for these sources ship transport will be less costly than pipeline transport.
c. The Rautaruukki steel plant in Bothnia Bay, Finland (case No 1 in Figure 1) emitted nearly 4.0 Mt in 2010 and has more than $1,000 \mathrm{~km}$ transport distance to the Faludden reservoir. Thus, from Figure 2 it can be concluded that also for this plant ship transport will be the least costly transport solution, since this plant has a transport distance exceeding 730 km .

Hence, for at least forty-five of the fifty-five sources with an annual capture potential of 0.5 Mt or more, ship transport will be the least costly transport option for each source individually. Consequently, for the remaining 10 sources, pipeline will be the least costly individual transport option, in most cases due to the short transport distance to the storage site.

### 3.2. Pipeline volumetric break-even point

Table 1 shows estimated $\mathrm{CO}_{2}$ captured based on plant $2010 \mathrm{CO}_{2}$ emissions and after having applied a capture ratio of $85 \%$, the calculated pipeline volumetric break-even point and the corresponding specific cost for pipeline transport from the eight hubs specified in Section 2 to the three selected storage sites (see Figure 1). For three of the hubs (Brevik, Lysekil and Hvidovre), the pipeline volumetric break-even point and corresponding cost is shown for transport both to the Gassum formation and to the southern parts of Utsira.

Table 1: Pipeline volumetric break-even point and associated cost for selected transport systems

| Case |  | Storage | Distance | Site Capture | Pipeline Volu | break-even point |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| no | Dispatch site | site | km | Potential, Mtpa | Volume Mtpa | Assc cost, $€$ /tonne |
| 1 | Rautaruukki steel | Faludden | 1,070 | 3.4 | NA | NA |
| 2 | Östrand Pulp \& Paper | Faludden | 730 | 1.2 | 5.3 | 14.0 |
| 3 | Naantali PP/Refinery | Faludden | 490 | 1.7 | 3.5 | 13.6 |
| 4 | Oxelösund SSAB steel | Faludden | 280 | 1.8 | 3.0 | 10.0 |
| 5a | Hvidovre Coal PP | Gassum | 420 | 2.5 | 3.0 | 13.0 |
| 5b | Hvidovre Coal PP | Utsira | 880 | 2.5 | 9.0 | 13.0 |
| 6a | Lysekil Refinery | Gassum | 165 | 1.5 | 1.2 | 16.0 |
| 6b | Lysekil Refinery | Utsira | 615 | 1.5 | 5.0 | 12.0 |
| 7 a | Brevik Cement | Gassum | 180 | 0.7 | 1.3 | 17.0 |
| 7b | Brevik Cement | Utsira | 560 | 0.7 | 4.0 | 13.0 |
| 8 | Nordic hub NW Jutl | Utsira | 490 |  | 3.5 | 13.6 |
| Site Capture Potential refers to capture from both fossil and biogenic sources at the site |  |  |  |  |  |  |
| NA: Pipeline more costly than ship irrespective of volume |  |  |  |  |  |  |

Table 1 indicates that ship transport will be the least costly transport solution for all the selected cases individually apart from case 6 a, i.e. from the Lysekil refinery to the Gassum storage site (bold font). It can therefore also be concluded that clusters (multiple capture sites) will be required from any of the selected hubs (apart from case 6a) for pipeline to be the least costly transport mode and, as evidenced in Section 3.1, for most of the sources located along the coast. However, it should be relatively easy to build up the volumes required for pipeline transport to be the least costly transport option from the Naantali site (case 3) and the Oxelösund site (case 4) provided the Faludden aquifer can be utilized for storage. The same applies to the Hvidovre site provided the Gassum formation can be utilized as a storage reservoir.

For Case 1, from Rautaruukki, Bothnia Bay, to Faludden, pipeline transport was calculated to have approximately the same cost as ship for volumes between 12 and 16 Mtpa while for all other volumes ship transport was the least costly transport option. This follows from the fact that for each 17 Mtpa of capacity we will have to add a new pipeline string to the system since we have set maximum pipeline diameter to 48 inches. One possible way to reduce the pipeline cost calculated in this work could be to install land based (or offshore) booster stations along the route. Booster stations (i.e. providing pressure increase) located on land (or on platforms) along the route would lead to that larger volumes could be transported through the pipeline and thus lead to reduced cost for the pipeline itself. Whether this also would lead to lower overall cost for the transport system when including the cost of landfall and booster stations (or platforms and booster stations) is outside the scope of this work.

### 3.3. Well injectivity and its potential effect on transport cost

In any reservoir there is an optimal $\mathrm{CO}_{2}$ injection volume, i.e. optimal with respect to full utilization of the storage capacity of the reservoir. Location of individual injection wells and water producers (for pressure management) as well as the $\mathrm{CO}_{2}$-volume that is injected per well are all important reservoir specific factors that will have an effect on the reservoirs ultimate storage volume. At the same time, drilling of offshore wells is expensive and it is therefore likely that each reservoir will have a specific injection strategy that will be balanced between cost and requirement for storage and injection capacity, see for instance [14, 15].

Drilling of offshore injection wells and water producers represent high costs while at the same time, as indicated in Section 3.1, the cost for ship transport of $\mathrm{CO}_{2}$ increases relatively slowly with increasing transport distance.

Also, little is known about the storage and injection capacity of the reservoirs in the Baltic Sea. Elforsk [8] states that suitable reservoirs in the southern Swedish sector of the Baltic Sea have relatively poor permeability and porosity characteristics but also that there may be reservoir intervals with better properties where higher injection rates could be safely achieved. According to [8], modelling suggests that 0.5 Mt could be injected per well and year through five injection wells in reservoirs in the Swedish part of the southern Baltic Sea. Mortensen et al. [10] report simulated injection of $\mathrm{CO}_{2}$ into the Faludden aquifer southeast of Gotland in the Baltic Sea assuming well injectivity between 0.5 and 1.0 Mt per year. The simulations include drilling of 6 injection wells and 5 water production wells [10].

Hence, it seems reasonable to assume an injectivity between 0.5 and 1.0 Mt per well and year in the Faludden aquifer when calculating how different injectivity levels in reservoirs in the Baltic Sea could affect a Nordic $\mathrm{CO}_{2}$ transport system. In order to analyze the effect injectivity may have on the choice of reservoirs in the Nordic region we calculated the transportation cost for four different assumptions on well injectivity (and consequently also on required number of wells and subsea templates) assuming that all cases transport 4 Mtpa of $\mathrm{CO}_{2}$ by pipeline or by ship from Naantaali, Finland (see Figure 1 and Table 1). Ship transport cost was calculated as specified in Chapter 2 but additionally, in order to include cost of injection, cost was calculated in two ways; optimizing ship sizes in order to achieve injection rates as close to the maximum as possible (to reduce "off-time" at the injection site as much as possible), i.e. close to 457 tons per hour ( $4 \mathrm{Mtpa} / 8,760$ hours), or by installation of an "injection barge" with and without an STL (Submerged Turret Loading) at the storage site. The size of the "injection barge" is assumed the same as the size of the transport ship.

Each system includes cost for drilling of injection wells including subsea templates and 4 km pipeline from each well head to the injection point. It is important to emphasize that cost only includes the transport system and drilling of the required number of wells including subsea templates with well heads. Costs for drilling water producers (for pressure management), for umbilicals and for reservoir monitoring have not been included. Table 2 shows the result assuming a total drilling cost of $€ 50$ million per injection well $[13,16]$.

Table 2: Specific cost ( $€$ /tonne) from Naantaali as function of injectivity

|  |  | Gassum (ship transport) |  |  | Utsira (ship transport) |  |  |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| Assumed well <br> injection capacity | Pipeline | Manipulating | Injection barge | Injection <br> barge | Injection <br> barge | Injection barge |  |
| Mtpa | Faludden | Ship size | no STL | with STL | Ship size | no STL | with STL |
| 0.5 | 28.5 | 37.1 | 37.0 | 37.4 | 38.4 | 35.4 | 3 |
| 1.0 | 19.5 | 27.6 | 25.4 | 25.8 | 28.4 | 26.8 | 27.2 |
| 2.0 | 15.7 | 22.1 | 22.0 | 22.4 | 25.6 | 22.6 | 23.0 |
| 4.0 | 13.7 | 19.3 | 19.2 | 19.6 | 23.7 | 20.7 | 21.1 |

Cost based on assumed drilling cost of $€ 50$ million per well [13].
As can be seen from Table 2, assuming a well injectivity of 0.5 Mtpa in Faludden indicates that it may be less costly to transport the $\mathrm{CO}_{2}$ by ship a further 800 km to Gassum and $1,300 \mathrm{~km}$ to Utsira provided that at least 1 Mt can be injected per well and year in Gassum/Utsira, in particular if an injection barge is moored at the injection site.

However, assuming that 1 Mt can be injected per well and year in Faludden reduces cost significantly implying that at least 4 Mt needs to be injected per well and year in Gassum for Gassum to be the least costly alternative while even higher injection rates will be required at Utsira. Yet, at these injection levels, the difference in cost between the three storage alternatives is modest, with cost ranging from $€ 19.2$ at Gassum to $€ 21.1$ at Utsira if an injection barge is moored at the site versus $€ 19.5$ at Faludden.

Reducing drilling cost per well by $50 \%$ to 25 million Euros changes the results slightly. Assuming a well injectivity of 0.5 Mtpa in Faludden will require the use of an "injection barge" and an injectivity of 1 Mtpa and well in Gassum for Gassum to be less costly while at least 2 Mt will have to be injected annually per well in Utsira in combination with the use of an "injection barge". Assuming instead that 1 Mt can be injected per well and year in Faludden will require use of an injection barge and an injection capacity of 4 Mtpa and well in Gassum for Gassum to be the least costly alternative.

Raising instead drilling cost per well by $50 \%$ to 75 million Euros yields that both Gassum and Utsira are less costly than Faludden at injectivity levels of 1 Mt per well and year assuming 0.5 Mt can be injected per well and year in Faludden. If Faludden has an injection capacity of 1 Mtpa and well, the results show that Gassum will need an injection capacity of at least 3 Mtpa and well and the use of an "injection barge" in order to be less costly than Faludden.

The calculations above emphasize that cost of drilling the wells may have a large impact on storage and transport systems and even more so if also water producers will have to be drilled. Thus the calculations show that reservoir injectivity may have a profound impact on $\mathrm{CO}_{2}$ transport systems in the Nordic region.

## 4. Discussion

Based on industrial experience and discussions with the industry we estimate that the cost calculations presented in this paper have an uncertainty level of $+/-35 \%$. Yet, this level of uncertainty is not likely to alter the main conclusions drawn from this study namely that ship transport is the least costly transport option in the Nordic region and that reservoir injectivity may potentially determine the type of transport system. The former is due to a combination of modest $\mathrm{CO}_{2}$-volumes and long transport distances for most of the sources in the region while the latter is caused by a combination of poor injectivity in the reservoirs in the Baltic Sea and the clear cost advantage for ship transport over long distances as illustrated in Figure 2.

Another uncertainty is of course the assumed injectivity levels in the Faludden aquifer in Section 3.3 (see Table 2). However, the main objective with the calculations in Section 3.3 is to show the potential effect for emission sources located along the Baltic Sea if it turns out that the Faludden aquifer and other aquifers in the region have a limited storage and injection capacity. Hence, a primary objective for implementation of CCS in Finland and Sweden should be to investigate further the storage capability of reservoirs in the Baltic Sea.

Transport cost for individual sources presented in this paper are higher than cost levels presented in other reports such as for instance in [17]. There are two main reasons for this, 1) the higher $\mathrm{CO}_{2}$-volumes and shorter transport distances applied in the ZEP report and 2) basic input assumptions such as 40 years project lifetime in [17] as opposed
to 25 years (of which only 23 years operational) applied in this work. The high transport cost calculated in this report will have a large impact on total cost for the whole CCS chain (capture, compression, transport and storage). Yet, as mentioned above, most large scale emission sources in the region are steel, cement, chemical and petrochemical plants and there are for the moment no other technology than CCS that can achieve substantial emission cuts from these industries, which was also recently emphasized by IEA [18].

ZEP [12] and Roussanaly et al., [19] reach conclusions similar to the conclusions reached in this work, namely that pipeline transport cost has significant scale benefits, ship transport cost increases only modestly with increasing distance and the transport distance where ship becomes less costly than corresponding offshore pipeline, increases with increasing transport volume. However, some results differ to the results presented in this work. In particular, [19] conclude that cost for ship transport is competitive at shorter distances than what is obtained in this work, for comparable volumes. Reasons for this are, among other factors, the shorter loading and unloading time applied in [19] and the $10 \%$ addition to the overall pipeline length (terrain factor) for pipeline only, whereas in this work a $10 \%$ addition has been applied for both pipeline and ship (cf Section 2).

It should be emphasized that some of the technologies required to discharge $\mathrm{CO}_{2}$ from a ship offshore still need to be demonstrated such as for example the handling of the cold $\mathrm{CO}_{2}$ prior to injection and positioning of the ship during injection, see for instance [12] and [20]. This could be solved either by heating the $\mathrm{CO}_{2}$ onboard the ship before injection or the $\mathrm{CO}_{2}$ could be loaded onto a floating storage barge moored at the injection site where the gas could be stored and heated prior to injection as suggested in Section 3.3 (see Table 2). However, in order to avoid offshore discharge from ship altogether, the ship could simply transport the $\mathrm{CO}_{2}$ to a land based hub from which a pipeline could transport the $\mathrm{CO}_{2}$ to the storage site, provided that this still is the least costly overall transport option [11].

Section 3.2 shows that most selected hubs would have to build up cluster systems in order to reach volumes required for pipeline to be the least costly transport alternative. The exception is Case 6a, i.e. the refinery at Lysekil assuming storage in the Gassum formation (see Table 1). An investor may of course still choose pipeline although this is not the economically optimal solution initially, i.e. if the investor is willing to carry the financial risk of underutilization of the pipeline for an unspecified period of time. The key question in this case will be who is willing to carry the financial risk of underutilization. One solution could be that the governments decide that public funding should help to carry the risk either singlehandedly or through some risk sharing. However, the risk of underutilization is one of the reasons why ship transport appears advantageous since this will allow for volumes to build up over time until such volumes have been reached that pipeline is the least costly transport mode (i.e. when the pipeline volumetric break-even point calculated in Section 3.2 and shown in Table 1 has been reached). Also, it should be emphasized that this work is limited to analysis of transportation systems. Yet, for the systems identified in this work to be viable, associated storage sites will need to be certified with accurate estimates of its storage capacity and injectivity including confirmation of its sealing capability. The certification process will obviously also require some level of risk taking (e.g. to determine who will carry the cost of drilling the wells that will be required to assess the storage and injection capacity of the reservoir).

There are regulatory obstacles remaining that may have an impact on the development of CCS and transportation of $\mathrm{CO}_{2}$ in the Nordic region such as transboundary transport of $\mathrm{CO}_{2}$, which is prohibited according to the London Protocol. Transboundary transport of $\mathrm{CO}_{2}$ is however exactly what will be required if the reservoirs in the Baltic Sea turn out to have a poor injectivity and/or storage capacity, i.e. if CCS is to become a viable solution to reduce emissions in Finnish and Swedish industries. Otherwise, the question arises if and how Finnish and Swedish industries can achieve substantial emission cuts without CCS. Another regulatory obstacle is that ship transport is not currently covered by the EUs Emission Trading System meaning that $\mathrm{CO}_{2}$ transported by ship and then stored still will be considered as emitted $\mathrm{CO}_{2}$ thereby making ship transport a non-viable solution [21]. The solutions to the regulatory obstacles mentioned above are not straightforward and the risk is that these obstacles may delay CCS with offshore storage (for a thorough review of the various legal obstacles with regard to CCS in the Nordic countries see [21].

## 5. Conclusions

In this paper we present results from an assessment of $\mathrm{CO}_{2}$ transportation options in the Nordic countries. Most of the stationary $\mathrm{CO}_{2}$ emissions in the Nordic region come from emission intensive industries such as steel, cement and
chemical industries and refineries characterized by many medium-sized and small emission sources and by large distances between individual sources and to potential storage sites.

Comparing cost for ship and pipeline transport as a function of volume and distance shows that ship transport is the least costly transport option not only for most of the sources in the region individually but also for most of the potential CCS clusters during ramp-up. This is due to the relatively modest $\mathrm{CO}_{2}$ volumes in combination with long transport distances and, for the case of clusters, the potential extra cost in connection with underutilized pipelines, in which case the use of ship transport should also reduce the financial risk taking. The results also show that cost for ship transport increases modestly with increasing distance.

The pipeline volumetric break-even point was calculated for eight selected cases (Cases 1-8) located along the coast in Denmark, Finland, Norway and Sweden assuming that local $\mathrm{CO}_{2}$-hubs could evolve on these sites. Thus, without speculating how a local hub can evolve over time with respect to $\mathrm{CO}_{2}$-volume, i.e. which sources will connect and when in time, these calculations simply render the volumes required for pipeline to be the least costly transport mode from that specific site. The results imply that cluster systems involving multiple sources will be required for most of the selected sites for pipeline to become the least costly transport mode. Also, for potential clusters evolving around the four sites situated along the Baltic Sea (Cases 1-4, i.e. Rautaruukki, Östrand, Naantaali and Oxelösund), pipeline transport will only be the least costly alternative if the $\mathrm{CO}_{2}$ can be stored in the Faludden aquifer for which there is currently only limited information on storage capacity available.

Based on the fact that cost for ship transport increases modestly with increasing distance and that injectivity in the Faludden aquifer may be low ranging from 0.5 to 1.0 Mt per year and well, it is shown in Section 3.3 that it could be less costly to instead transport the $\mathrm{CO}_{2}$ by ship $800-1,300 \mathrm{~km}$ further to the west to storage in Gassum or Utsira. Thus, injectivity may have a profound effect on $\mathrm{CO}_{2}$ transport and storage systems in the Nordic region.

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