# Kinetic modeling of H<sub>2</sub>-assisted C<sub>3</sub>H<sub>6</sub> Selective Catalytic Reduction of NO over Silver Alumina catalyst

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#### Results and discussion

A sample of experimental and simulation results:

- Ag/Al<sub>2</sub>O<sub>3</sub> catalyst is a potential catalyst for NO<sub>x</sub> abatement with HC-SCR technology. Further, addition of H<sub>2</sub> has been shown to give better HC-SCR performance on Ag/Al<sub>2</sub>O<sub>3</sub>[1].
- The present work aims to set up a global kinetic model to describe mechanistic role of H<sub>2</sub> to promote C<sub>3</sub>H<sub>6</sub>SCR over Ag/Al<sub>2</sub>O<sub>3</sub> catalyst.

#### Experimental methods

- Ag/Al<sub>2</sub>O<sub>3</sub> with 2 wt.% Ag loading was prepared by sol-gel freeze dried method. The catalyst powder was washcoated on cordierite monolith.
- Activity measurement was conducted in a flow reactor equipped with gas FTIR and MS.
- Temperature-programmed reaction and transient experiments were used.
- The model aimed to simulate wide range of temperature and inlet feed concentration.







### Modeling methods

Development of reaction mechanisms:

- Experimental data shows NO oxidation and C<sub>3</sub>H<sub>6</sub> SCR are always higher in the presence of H<sub>2</sub> even for high temperature range.
- Initial screening of mechanisms suggested that single role of H<sub>2</sub> to remove inhibiting nitrate was insufficient to reproduce wide ranging experimental conditions.
- Key point in reaction mechanism: H<sub>2</sub> is proposed to have dual role to remove inhibiting nitrate and simultaneously form more active reduced sites, S<sub>2</sub>.



Temperature-programmed reaction of H2-assisted C3H6 SCR.Transient experiment by varying H2 concentration inFeed: 500 ppm NO, 8% O2, 1000 ppm C3H6, 0.1% H2 and 5% H2O. $C_3H_6SCR$  at 375°C. Feed: 500 ppm NO, 8% O2, 1000 ppm C3H6, 0.1% H2 and 5% H2O. $C_3H_6$ , 0 to 2000 ppm H2 and 5% H2O.

- The proposed H<sub>2</sub> role reproduced experimental data well for both temperatureprogrammed and transient experiments. Similarly, model validation under NO, C<sub>3</sub>H<sub>6</sub> oxidation and C<sub>3</sub>H<sub>6</sub> SCR with/without H<sub>2</sub> at 250 and 400°C gave good agreement between simulations and transient experiments.
- All reactions on reduced Ag sites (S<sub>2</sub>) are more rapid than on oxidized Ag sites (S<sub>1</sub>) which is indicated by lower activation energies on S<sub>2</sub> than on S<sub>1</sub> for the same reactions.
- Weisz modulie evaluations were made for H<sub>2</sub>-assisted C<sub>3</sub>H<sub>6</sub> SCR and C<sub>3</sub>H<sub>6</sub> SCR indicated that larger fraction of experimental data was free from mass transport resistance.

- $C_{3}H_{6}$  and  $H_{2}$  oxidation with NO<sub>2</sub>
- Reactor model: single channel model was used to describe mass transfer and reaction kinetic. The model also includes mass transfer of gas components inside washcoat [2].

### References

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A global kinetic model for H<sub>2</sub>-assisted C<sub>3</sub>H<sub>6</sub> SCR has been developed to effectivey capture a wide range of feed concentrations and temperature.
The model proposes dual role of H<sub>2</sub> to eliminate nitrate as well as to form a reduced sites, S<sub>2</sub>. NO oxidation, H<sub>2</sub> oxidation as well as C<sub>3</sub>H<sub>6</sub> SCR reactions are more rapid on the reduced sites, S<sub>2</sub>.
A larger fraction of experimental data was free from the influence of mass

transport resistance.



