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Balanced globin protein expression and heme biosynthesis improve production of human hemoglobin in *Saccharomyces cerevisiae*

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26 **Abstract**

27

28 Due to limitations associated with whole blood for transfusions (antigen compatibility, transmission of
29 infections, supply and storage), the use of cell-free hemoglobin as an oxygen carrier substitute has
30 been in the center of research interest for decades. Human hemoglobin has previously been
31 synthesized in yeast, however the challenge is to balance the expression of the two different globin
32 subunits, as well as the supply of the prosthetic heme required for obtaining the active hemoglobin
33 ($\alpha_2\beta_2$). In this work we evaluated the expression of different combinations of α and β peptides and
34 combined this with metabolic engineering of the heme biosynthetic pathway. Through evaluation of
35 several different strategies we showed that engineering the biosynthesis pathway can substantially
36 increase the heme level in yeast cells, and this resulted in a significant enhancement of human
37 hemoglobin production. Besides demonstration of improved hemoglobin production our work
38 demonstrates a novel strategy for improving the production of complex proteins, especially multimers
39 with a prosthetic group.

40

41 **Key words**

42 Human hemoglobin, heme biosynthesis, prosthetic group, protein production, *Saccharomyces*
43 *cerevisiae*

44

45

46 **1. Introduction**

47 Hemoglobin is the major oxygen transport protein in blood and is found in erythrocytes. The protein is
48 a tetrameric metalloprotein consisting of four globin subunits ($\alpha_2\beta_2$) with each subunit containing a
49 prosthetic heme group. One heme molecule is comprised of a protoporphyrin IX and a ferrous iron
50 which has high affinity for binding oxygen (Belcher et al., 2010; Benesch and Benesch, 1963). Due to
51 the concerns with whole blood for transfusion, e.g. limited resources, cross-typing requirements and
52 transfusion transmitted disease, substantial efforts have been put into the development of safe and
53 effective human blood substitutes (Looker et al., 1992; Wagenbach et al., 1991). Aside from synthetic
54 perfluorocarbon (PFC) polymers (Biro, 1993) and erythrocyte products (which are purified
55 hemoglobin from a variety of mammalian sources), cell-free hemoglobin-based oxygen carrier (HBOC)
56 has been extensively studied for its high efficiency in oxygen transfer and its contribution to the
57 maintenance of osmotic pressure (Lu et al., 2011). The main limitation with this product is protein
58 instability due to tetramer dissociation into dimers, resulting in short retention time and renal toxicity,
59 and high oxygen affinity in the body caused by absence of a co-factor 2, 3-bis (phospho) glycerate
60 (2,3-BPG) (Kroeger and Kundrot, 1997; Looker et al., 1992; Wagenbach et al., 1991). A series of
61 advances have been achieved including chemical modifications of natural hemoglobin to extend its
62 half-life in circulation (Harris and Palmer, 2008) which have greatly stimulated further studies on
63 HBOC (Lu et al., 2011).

64

65 With the development of recombinant DNA technology, it became possible to engineer hemoglobin
66 with genetic engineering, which enabled designed modification to improve its biological properties as
67 well as to enhance its production. A variety of strategies have been applied in different organisms
68 since the late 80s ranging from bacteria (Hoffman et al., 1990) to higher organisms, including plants
69 (Dieryck et al., 1997) and animals (Behringer et al., 1989; Martinez et al., 2012). The main advances
70 include (i) expression of α and β globin chains simultaneously and refold together, with addition of
71 exogenous heme *in vitro* (Hoffman et al., 1990) (ii) Co-expression of the methionine amino-peptidase
72 (Met-AP) gene with the globin genes to reduce the N-terminal methionine in modified globins

73 produced in *E. coli* (Shen et al., 1993) (iii) Site-directed mutations in β globin chain in order to reduce
74 the extreme oxygen affinity due to the lack of 2,3-BPG allosteric regulation (Hernan et al., 1992) (iv)
75 Tandem fusion of two α globins to prevent tetramer disassociation into $\alpha\beta$ dimers (Looker et al., 1992)
76 (v) Co-expression of bacterial heme membrane transporter systems to increase heme uptake and
77 further enhancement of hemoglobin production (Graves et al., 2008). In addition to this, several recent
78 studies showed that α -hemoglobin stabilizing protein (AHSP) could prevent α globin precipitation and
79 hereby have a positive effect on hemoglobin production (Feng et al., 2004; Feng et al., 2005; Vasseur-
80 Godbillon et al., 2006).

81

82 The yeast *Saccharomyces cerevisiae* is a well-known cell factory for production of fuels (Lee et al.,
83 2008), chemicals (Chemler et al., 2006; Nevoigt, 2008) and heterologous proteins, especially industrial
84 enzymes and pharmaceuticals (Hou et al., 2012; Martinez et al., 2012). There are several reasons why
85 yeast can potentially be a highly competitive expression host for production of human hemoglobin: it
86 is general regarded as safe (GRAS organism) which avoids the risk of pathogen contaminations from
87 human or animal resources, it is able to perform post-translational modifications, including correct
88 processing the globin termini, folding and subunit assembling (Porro et al., 2005), being the
89 prerequisite for proper reconstitution of a soluble heme-containing tetramer *in vivo*. Furthermore,
90 being a long-term eukaryal model organism, numerous studies have been carried out on *S. cerevisiae*
91 from which extensive genome and physiological information have been generated (Petranovic and
92 Nielsen, 2008). For these reasons several recombinant proteins such as human insulin (Novo Nordisk),
93 human bovine serum albumin (Novozymes) and hepatitis vaccines (GlaxoSmithKline, Merck) among
94 others, have been industrially produced and approved for medical applications in *S. cerevisiae*
95 (Martinez et al., 2012; Walsh, 2010).

96

97 Hemoglobin synthesis is highly conserved through evolution and the non-globin part, the prosthetic
98 group protoporphyrin IX, is common among divergent species such as human and yeast, so one can
99 utilize the endogenous yeast heme pathway for the production of human recombinant hemoglobin
100 (Kumar, 1995). Studies suggest that recombinant hemoglobin produced in yeast remains fully

101 functional and shows identical rate of dissociation as the native human hemoglobin (Coghlan et al.,
102 1992). However, with improved globin production it is questionable whether endogenous heme
103 production is sufficient. Thus, it has been found that supplementation with hemin can accelerate
104 hemoglobin synthesis in immature cultured erythroid cells, which suggests that heme availability is a
105 rate-controlling step for hemoglobin production (Fibach et al., 1995). Additionally, heme association
106 to globins was suggested to occur co-translationally and could therefore facilitate the formation of the
107 proper tertiary structure on the ribosome (Komar et al., 1997). A coordinated optimization of
108 endogenous heme level is therefore expected to improve heterologous hemoglobin production in yeast
109 cells.

110

111 The heme biosynthesis pathway in yeast (Figure 1) contains eight steps starting from 5-aminolevulinic
112 acid (ALA) synthesis from succinyl-CoA and glycine (catalyzed by Hem1p) in mitochondria. After
113 being transported to the cytosol to form porphobilinogen (PBG) (catalyzed by Hem2p), the
114 intermediate is further converted to hydroxymethylbilane (catalyzed by Hem3p) and then
115 uroporphyrinogen III (by Hem4p) and finally into coproporphyrinogen III (catalyzed by Hem12p).
116 The coproporphyrin III is transported back to the mitochondria and converted to protoporphyrinogen
117 IX by Hem13p following synthesis of protoporphyrin IX (by Hem14p). The last step is the
118 incorporation of an iron atom into protoporphyrin IX to form the heme molecule catalyzed by Hem15p.

119

120 In this study, we evaluated the effect of metabolic engineering the heme biosynthetic pathway on
121 heterologous hemoglobin production (Figure 1): we overexpressed, individually or in different
122 combinations (with promoters of different strengths), three genes coding for enzymes that represent
123 confirmed (*HEM2* and *HEM3*) or suspicious (*HEM12*) rate-limiting steps in the heme biosynthetic
124 pathway (Hoffman et al., 2003), and additionally co-expressed α and β globin genes in different ratios.
125 Using this approach we could evaluate a large number of combinations with engineering the heme
126 biosynthesis and globin subunit co-expression and hereby identify the optimal combination for high
127 level human hemoglobin production.

128

129 **2. Materials and Methods**

130 **2.1. Plasmids and strains**

131 *S. cerevisiae* CEN.PK 113-11C (*MATa his3Δ1 ura 3-52 MAL2-8c SUC2*)(Entian and Kötter, 1998)
132 was used as the host strain for all the experiments performed in this study. Plasmid constructions were
133 performed following standard molecular biology techniques using *Escherichia coli* DH5α (Bethesda
134 Research Laboratories). All yeast transformations were performed following standard lithium acetate
135 method (Daniel Gietz and Woods, 2002) and selected on synthetic dextrose media SD-His (heme
136 overexpression strains), SD-Ura (globin overexpression strains), and SD-His-Ura (heme and globin
137 double overexpression strains) respectively. For cultivation, yeast strains were grown in liquid SD-His,
138 SD-Ura and SD-His-Ura accordingly.

139

140 All the heme overexpression plasmids were constructed using a bidirectional expression plasmid
141 pIYC04 (Chen et al., 2013). The heme genes were amplified from the chromosomal DNA of CEN.PK
142 113-11C (Table S1). Plasmids H2, H3 and H12 were constructed by inserting the corresponding genes
143 into the expression cassette of pIYC04 under the *TEF1* promoter. Plasmids H2H3 and H2H12 were
144 constructed by inserting *HEM3* and *HEM12* respectively into H2 under the *PGK1* promoter.
145 H3H2H12 was built by inserting a *HEM3* expression cassette amplified from H3 into H2H12. The
146 globin overexpression plasmids were constructed from a different bidirectional expression plasmid
147 pSP-GM1 (Chen et al., 2012). The DNA sequences (with restriction sites at both ends), namely *HBA*
148 (coding α), *HBB* (coding β) and *HBAA* (coding di-α) were synthesized by GeneScript, Inc., and codon
149 optimized to facilitate their expression in *S. cerevisiae*. The *HBAA* sequence coding di-α was made by
150 linking two *HBA* gene sequences (first one without stop codon) with one glycine linker. The *HBB*
151 fragment was digested with *SalI* and *KpnI* and ligated under the *PGK1* promoter of pSP-GM1 first.
152 Then the *HBA* and *HBAA* fragments were digested by *NotI* and *SacI* and ligated under the *TEF1*
153 promoter of pSP-GM1 to make B/A and B/AA respectively. Plasmid B/A/A was made by inserting the
154 *HBA* expression cassette amplified from B/A into plasmid B/A between *PstI* and *MfeI*. Plasmid
155 B/AA/B was constructed by inserting the *HBB* expression cassette amplified from B/A into the *MfeI*

156 site of plasmid B/AA. All the primers and the synthesized globin gene sequences are listed in the
157 supplementary file (Table S1, S2).

158

159 CEN.PK 113-11C was transformed with the heme and globin overexpression plasmids, resulting in
160 different recombinant host strains (Figure 1B, Table 1).

161

162 **2.2. Coproporphyrin assay**

163 Coproporphyrin levels were measured by HPLC using the HPLC Porphyrin Kit from ALPCO
164 Diagnostics Inc. Strains transformed with the heme overexpression plasmids were cultured in SD-His
165 (containing 6.7 g/L of yeast nitrogen base w/o amino acids (Difco Laboratories, Sparks, MD), 0.77 g/L
166 of complete supplement mixture (CSM, w/o histone) (MP Biomedicals, Solon, OH) and 2% glucose)
167 medium at 30°C with constant shaking at 180 rpm during 96 hours before being harvested. Cell pellets
168 collected from 35ml of culture were resuspended into 1mL of 0.6% HCl after being washed twice with
169 ddH₂O. The suspended cell pellets were kept in dark at 4 °C before being loaded onto HPLC (PU-2089
170 Plus pump, AS-2057 Plus auto sampler, and FP-920 fluorescence detector, JASCO). The eluents,
171 standard, and reversed phased C₁₈-column were included in the kit and the running conditions were
172 referred to the kit.

173

174 **2.3. Heme/porphyrin determination assay**

175 The intracellular heme concentration was measured using a protocol derived from (Sassa, 1976) and
176 slightly modified from (Michener et al., 2012). Cells were grown to a desired density and harvested at
177 OD₆₀₀*mL =8 (e.g. if OD₆₀₀=2, 4mL of culture is harvested). The cell pellets were resuspended in
178 500µL of 20mM oxalic acid and then kept in dark at 4 °C overnight. 500µL of preheated 2M oxalic
179 acid was added and half of the mixture was taken into an amber tube and heated up to 95-98 °C for 30
180 minutes during which the other half mixture was kept at room temperature. 200µL of clear supernatant
181 was transferred into a black 96 plate and fluorescence with excitation at λ= 400nm and emission at λ=
182 600nm was monitored. The total porphyrin level (bound heme and free porphyrins) corresponds to the
183 heated sample, and the free porphyrins level corresponds to the non-heated sample.

184

185 **2.4. SDS-PAGE assay**

186 For protein extraction, yeast cell samples were taken at the indicated times and cells were harvested by
187 centrifugation. Pellets were resuspended in 2ml of NaOH containing 7% 2-mercaptoethanol plus 2ml
188 of trichloroacetic acid (TCA) and incubated 2 min at room temperature. After incubation, cells were
189 washed with 1M Tris-HCl (pH 7.5) and centrifuged. The cell pellet was resuspended in loading buffer
190 (SDS 3%, Glycerol 10%, 2-mercaptoethanol 5%, Tris pH 6.8 0.0625 M, 0.01 mg bromophenol blue)
191 and heated up to 95°C during 5 min. Cells were discarded by centrifugation and the remaining protein
192 suspension was used for loading into gradient (4-12%) polyacrylamide bis-tris gels (Novex, Invitrogen)
193 at the selected protein concentrations. The marker ladder used was Novex Sharp Pre-stained Protein
194 Standard from Invitrogen. Software GelPro Analyzer (Media Cybernetics) was used for quantification
195 of band intensities.

196

197 **2.5. Assay for active hemoglobin**

198 Washed cell pellets were resuspended into 500µl of 100mM of PBS buffer supplemented with 1x
199 protease inhibitor (Halt Protease Inhibitor Cocktail, Thermo), pH 7.0. The cell suspension was loaded
200 into a FastPrep™ Lysing tube with an equal volume of glass beads (425-600µm diameter, Sigma).
201 Cells were broken by applying 8 pulses of 20 seconds with the speed of 6m/s using a FastPrep 24
202 instrument (MP, Biomedicals, LLC). The sample tubes were placed on ice for 3 minute between pulses.
203 Clear supernatants were harvested by centrifugation at full speed for active hemoglobin assay and
204 protein quantification. Lipid removal agent Cleanascite (X2555-100, BIOTECH SUPPORT GROUP)
205 was added according to product description in case of unclear suspensions in the supernatant. Protein
206 concentration was measured by BCA protein assay kit (Cat 23225, Pierce). The active hemoglobin was
207 measured using the QuantiChrom™ Hemoglobin Assay Kit (DIHEMOGLOBIN-250, Clonagen),
208 based on an improved Triton/NaOH method, in which the hemoglobin is converted into a uniform
209 colored end product that can be measured by spectrophotometer.

210

211 **2.6. Relative gene transcription levels by qPCR**

212 Yeast cells were cultured at 30°C with shaking at 180 rpm in shake flask containing 50 ml of SD-His.
213 Total RNA was isolated from 10 ml of cells with OD₆₀₀ around 1. The cells were disrupted by Fast-
214 Prep 24 (MP-Biomedicals) using glass beads (Lysing matrix C, MP-Biomedicals). Extracted RNA was
215 purified using the RNeasy kit (Qiagen). 200 ng of total RNA was used to synthesize cDNA from
216 which 2 µl of the synthesized cDNA was used as the template for the qPCR reaction to a final reaction
217 volume of 20 µl, using the Brilliant III Ultra Fast SYBRGreen QPCR Master mix (Stratagene) in
218 Mx3005P QPCR System (Agilent Technologies). Cycle thresholds (Ct) were normalized to the Ct
219 value of *S. cerevisiae ACT1*.

220

221 **2.7. Batch fermentations**

222 Fresh colonies were picked to inoculate into 50 mL of SD- His-Ura media (containing 6.7 g/L of yeast
223 nitrogen base w/o amino acids (Difco Laboratories, Sparks, MD), 0.75 g/L of complete supplement
224 mixture (CSM, w/o histone and uracil) (MP Biomedicals, Solon, OH) and 2% glucose) to make seed
225 cultures. After growing for 24 hours at 30°C at 180 rpm, the seed cultures were inoculated into the
226 bioreactors with an initial OD₆₀₀ of 0.1. Fermentations were performed in DasGip 1.0-liter stirrer-pro
227 vessels (DASGIP GmbH, Germany) with a working volume of 600 mL in SD -His-Ura media. The
228 temperature was controlled at 30°C with agitation at 600 rpm and aeration at 1 vvm. Dissolved oxygen
229 was controlled above 30% throughout the experiment. The impeller speed was automatically adjusted
230 in response to the sensor. The pH was maintained at 6.0 using 2M KOH in response to the pH sensor
231 (Mettler Toledo, Switzerland). All fermentations were performed in biological duplicates. Dry cell
232 weight was measured by filtering 5mL of cell culture through a 0.45µm filter membrane and
233 calculating the increased weight of the dried filter. Supernatants filtered through 0.45µm membrane
234 were loaded to HPX-87G column (BIORAD, USA) on a Dionex Ultimate 3000 HPLC (Dionex
235 Softron GmbH, Germany) to measure the concentrations of glucose, ethanol, and glycerol in the
236 cultures. The samples were running with a flow rate of 0.6mL/min at 65°C using 5mM H₂SO₄ as
237 mobile phase.

238

239 **Results and Discussion**

240

241 To investigate the impact of increased endogenous heme synthesis on heterologous hemoglobin
242 production in *S. cerevisiae*, a series of recombinant strains were constructed by transforming different
243 expression plasmids in the yeast strain CEN.PK 113-11C (Fig 1, Table 1).

244

245 ***3.1. Increased endogenous heme level by overexpression of heme genes***

246 By transforming the heme overexpression plasmids H2, H3, H12, H2H3, H2H12, and H3H2H12 into
247 CEN.PK 113-11C, strains with the engineered heme biosynthesis pathway were constructed (Table 1).
248 The strains were designated with the same names as the corresponding plasmids H2, H3, H12, H2H3,
249 H2H12, and H3H2H12 (Table 1). The cytosolic intermediate of the heme biosynthetic pathway,
250 coproporphyrin was measured in all the engineered strains and used as an indicator for heme and
251 porphyrin levels in the cells (Fig 2A). All strains were compared with the strain transformed with
252 pIYC04 (empty plasmid) and the fold values were calculated relative to it. Strain H3 showed a four
253 times increase on coproporphyrin level compared to the control strain, pIYC04, followed by H12 and
254 H3H2H12 whose coproporphyrin levels were 3.2 and 2.2 times to pIYC04 respectively (Fig 2A). In
255 terms of bound heme level, H3 still stood out with almost 5 fold of pIYC04, followed by H3H2H12,
256 2.8 fold, and H12, 2.4 fold (Fig 2B).

257

258 *HEM13* transcription is known to be negatively regulated by oxygen and heme (Zagorec and Labbe-
259 Bois, 1986) through *HAPI* and *ROX1* (Keng, 1992). Overexpression of the genes in the heme
260 biosynthesis pathway (strains H2, H3, H12, H2H3, H2H12 and H3H2H12) resulted in certain
261 improvements on heme levels (Fig 2B) which might induce feedback inhibition on the synthesis of
262 Hem13p which converts coproporphyrinogen III into protoporphyrinogen IX, causing subsequent
263 accumulation of coproporphyrins (Michener et al., 2012). The coproporphyrin levels (Fig 2A) may
264 therefore represent reliable indicators of the heme levels in the strains, and Hem13p might be another
265 potential bottleneck in addition to the reported rate-limiting steps catalyzed by Hem2p and Hem3p.

266 Both driven by *TEF1* promoter, *HEM3* overexpression (H3) showed a better effect than *HEM12*
267 overexpression (H12) on coproporphyrin accumulation suggesting a greater rate-limiting effect of
268 Hem3p than Hem12p during heme biosynthesis. Overexpression of *HEM3* released the bottleneck in
269 this step providing more intermediate for further (catalyzed by Hem4p and Hem12p) conversion to
270 coproporphyrin. On the other hand, also driven by the *TEF1* promoter, *HEM2* overexpression (H2)
271 exhibited a very limited improvement on the coproporphyrin level in the cells although the Hem2p has
272 been confirmed as a rate-controlling enzyme under aerobic conditions (Hoffman et al., 2003; Zhang
273 and Hach, 1999). This is very likely due to the enzymes blocking the subsequent steps, especially
274 Hem3p and Hem12p, were not overexpressed in H2. The point could be supported by the higher
275 coproporphyrin levels presented in H2H3 and H2H12 than in H2. Since *HEM3* in H2H3 and *HEM12*
276 in H2H12 are both under the *PGK1* promoter which has a reported weaker strength than *TEF1*
277 promoter (Valérie Nacken, 1996) driving *HEM2* in these strains, the steps catalyzed by Hem3p and
278 Hem12p may still being blocked to certain extends which could partly explain the not so obvious
279 improvements on the coproporphyrin levels in these strains. Additional reason could be that with more
280 gene cassettes compulsory for expression, the resource for expressing one gene has to be distributed to
281 more genes and therefore each gene gets lesser/weaker expression. The expressions of *HEM2*, *HEM3*
282 and *HEM12* in H2H3 and H2H12 might have been reduced to certain levels resulting in the minor
283 improvement of coproporphyrin accumulation than H2. Similarly, the expression burden was even
284 heavier for the cells in the H3H2H12 strain and consequently the proteins especially Hem3p which has
285 been indicated to be the most effective enzyme compared to Hem2p and Hem12p to block heme
286 synthesis, were less expressed, which could be the reason that H3H2H12 did not show higher or even
287 comparable level of coproporphyrin than H3 and H12.

288

289 The transcriptional levels of *HEM3* and *HEM12* were examined and as shown in Fig 3, the mRNA
290 levels of the heme genes *HEM3* and *HEM12* were much higher in the strains transformed with the
291 corresponding vectors than with the empty vector. The transcriptional level of *HEM3* in strain H3 is
292 extremely high (131.6 folds) correlating to the highest coproporphyrin accumulation in the H3 strain.

293

294 The acidic-heat method can discriminate between heme bound to proteins and the free porphyrins in
295 cells. As shown in Fig 2B, the heme level in H3 was the most abundant followed by H3H2H12 and
296 H12, showing the same trend as that for coproporphyrin. The higher heme level in H3 than in H12
297 might indicate a bigger flux of coproporphyrins converted to protoporphyrin IX than in H12, even
298 though the coproporphyrins accumulated in H3 were also more than in H12. The free porphyrins
299 include more than coproporphyrins which might explain the higher free porphyrin levels in H12
300 compared to H3. Both assays indicate that *HEM3* overexpression alone generates the highest heme
301 levels in cells compared to the other strains.

302

303 ***3.2. Co-overexpression of heme and globin constructs increased heterologous hemoglobin*** 304 ***production***

305 The top three heme overexpression plasmids H3, H3H2H12 and H12 were selected to be co-
306 transformed together with a range of globin overexpression plasmids B/A, B/AA, B/AA/B, B/A/A and
307 the empty vector pSP-GM1 (Fig 1B). The combination of α and β globin genes on the globin vectors
308 were designed based on i) α globin is more unstable than β globin (Vasseur-Godbillon et al., 2006) and
309 ii) $\alpha\beta$ dissociation can be prevented by linking two α globin genes with a glycine linker (Looker et al.,
310 1992). The expression levels were examined by SDS-PAGE (Fig 4). By co-overexpression with H3,
311 the globin construct B/A/A showed the highest protein expression, however, there was nearly no band
312 of the right size (around 16 KDa) when H3 was expressed in combination with other globin constructs
313 (Fig 4A). Very weak signal of α and β globins were detected by ELISA (data not shown) and based on
314 this result, co-overexpressions of B/A/A with the other two heme overexpression plasmids H12 and
315 H3H2H12 were also checked by SDS-PAGE: with heme overexpressed, the globin synthesis was also
316 improved (Fig 4B). Expression of B/A/A with the empty plasmid pIYC04 did not show clear
317 expression, thus further supporting the hypothesis that endogenous heme levels are insufficient to
318 achieve high heterologous globin production (Smith et al., 2011).

319

320 ***3.3. Effect of B/A/A co-overexpression on heme/porphyrin level***

321 In order to understand if an improved hemoglobin expression is correlated with an increased heme
322 level, the heme/porphyrin level in the strains co-overexpressed with B/A/A was examined.

323

324 The relative fold change was calculated relative to the heme level in pIYC04+pSP-GM1. As shown in
325 Fig 5, both the bound heme level and the free porphyrins level in H3+B/A/A are higher than in
326 H3+pSP-GM1, and in the H3H2H12+B/A/A strain compared with H3H2H12+pSP-GM1. With B/A/A
327 co-overexpressed, we found an increase of 87% with H3 co-overexpression. In erythroid cells, heme
328 export from the mitochondria requires a corresponding synthesis of heme-binding proteins (Lynch et
329 al., 2009). One hypothesis could be that with higher levels of globin expressed, an initial decrease in
330 the pool of free cytosolic heme occurs which induces an increase in the production rate of porphyrins
331 resulting in a global increase of both free porphyrins and consequently the hemoproteins. The bound
332 heme levels that we measured would be thus higher.

333

334 ***3.4. Physiological characterization and active hemoglobin production in batch fermentations***

335 The physiological properties of the recombinant hemoglobin strains were characterized in batch
336 fermentations, as shown in Table 2. The specific growth rates did not vary significantly which were
337 0.25, 0.28, 0.28 and 0.27 respectively for H3+B/A/A, H3H2H12+B/A/A, pIYC04+B/A/A and
338 pIYC04+pSP-GM1. At the end of cultivation, the percentages of the active hemoglobin in the whole
339 extracted soluble proteins were assayed and calculated. The result showed that the strain H3+B/A/A
340 had the most active hemoglobin accounting for 4.09% of the whole cell soluble protein followed by
341 H3H2H12+B/A/A with 3.82%. There was activity accounted for 2.8% of the whole cell protein in the
342 pIYC04+pSP-GM1 strain, most probably contributed by the endogenous flavohemoglobin (Zhao et al.,
343 1996).

344

345 The specific growth rate of strain H3+B/A/A was slightly lower when compared with other strains. It
346 also had the most soluble hemoglobin production and less biomass yield. Declines on specific growth
347 rate due to plasmid-encoded recombinant gene expression have been extensively noticed in bacteria,
348 yeast and filamentous fungi (Hoffmann and Rinas, 2004; Pakula et al., 2005; Tyo et al., 2012) all

349 pointing to a higher stress and impairment to cellular process. In the strain H3+B/A/A, a coordinated
350 over production of heme and globin units have been achieved which further assembled to the correct
351 tetramer. This process might result in a flux switching from normal cellular processes to recombinant
352 hemoglobin production, and consequently affect cell performance. The heme and globins production
353 is less effective in the other two recombinant strains thus the normal growth have not been impaired
354 significantly.

355

356 The cell growth reached the end of the glucose phase and the beginning of the ethanol phase at around
357 20 and 36 hours after inoculation respectively (Fig 6A). Interestingly, we found that the heme level in
358 H3+B/A/A significantly decreased before the ethanol phase started (Fig 6B) indicating a negative
359 correlation between heme/porphyrin synthesis and respiration. In contrast, in H3H2H12+B/A/A and
360 pIYC04+pSP-GM1, the heme level kept improving after the glucose phase was finished with a
361 decrease in the free porphyrin level suggesting that porphyrin synthesized in the glucose phase were
362 gradually converted into heme. The correlation between the heme levels and the hemoglobin
363 production was also measured by SDS-PAGE (Fig 6C). Clearly, the level of hemoglobin produced in
364 the glucose phase is higher than in the beginning of the ethanol phase (about 1.3 fold) for H3+B/A/A,
365 confirming that efficient heterologous hemoglobin production requires a low rate of respiration, as it
366 occurs during the glucose consumption phase in the fermentation process.

367

368 **Conclusion**

369 Previous studies have reported successful expression of recombinant human hemoglobin in the yeast *S.*
370 *cerevisiae* (Adachi et al., 1992; Coghlan et al., 1992; Martin de Llano et al., 1993; Ogden et al., 1994;
371 Wagenbach et al., 1991). In this study, yeast heme synthesis pathway was engineered for the first time
372 to facilitate the synthesis of recombinant hemoglobin, resulting in an increase of 1.3 times (H3+B/A/A
373 against pIYC04+B/A/A) in hemoglobin production. This work has generated a plasmid platform for
374 further improving heterologous hemoglobin production in yeast. Further improvement might be
375 achieved by engineering the heme membrane transport and/or the iron trans-membrane pathway (e.g.
376 ferric reductase and permease-oxidase complex required for iron uptake in *S. cerevisiae*) (Dancis et al.,
377 1990; Ginzburg et al., 2009; Graves et al., 2008; Stearman et al., 1996; Villarreal et al., 2008). In
378 addition to hemoglobin, a similar strategy can be applied to enhance the production of other
379 hemoproteins, e.g. cytochromes, catalases and P450 enzymes which are powerful catalysts for
380 synthesis of drug metabolites (Jung et al., 2011). This work is further demonstrating the possibility for
381 efficient production of complex proteins (e.g. multimer with a prosthetic group), as we have
382 demonstrated that the production of a prosthetic group can be increased through metabolic engineering
383 and hence eliminate the need for exogenous supplementation with expensive precursors.

384

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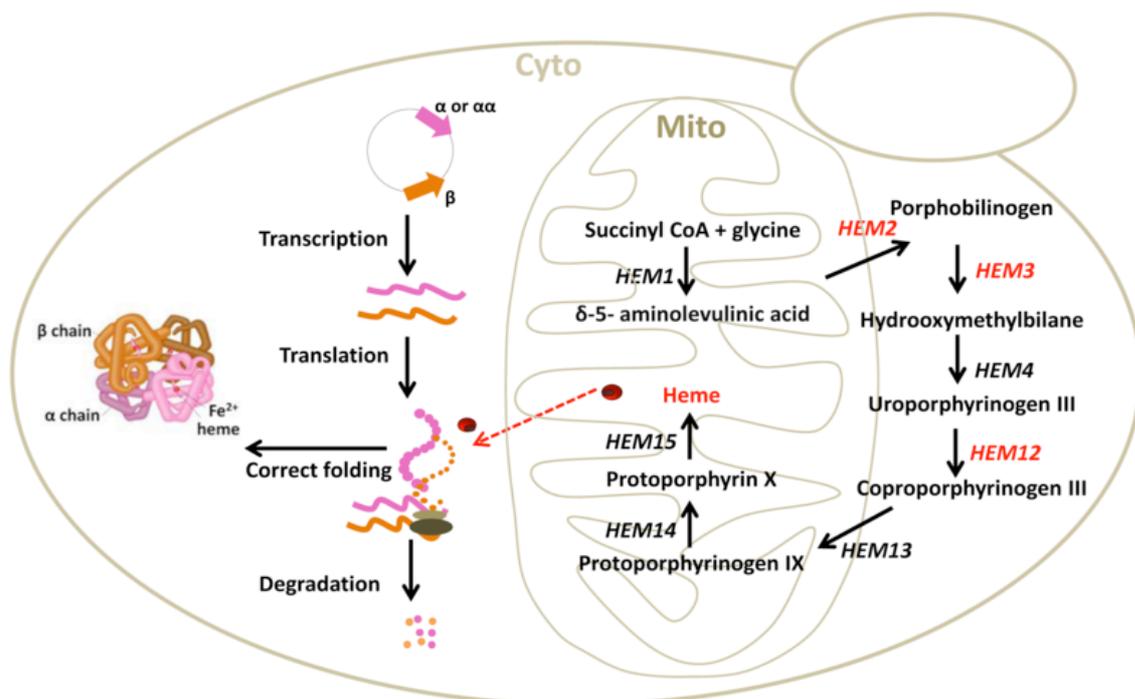
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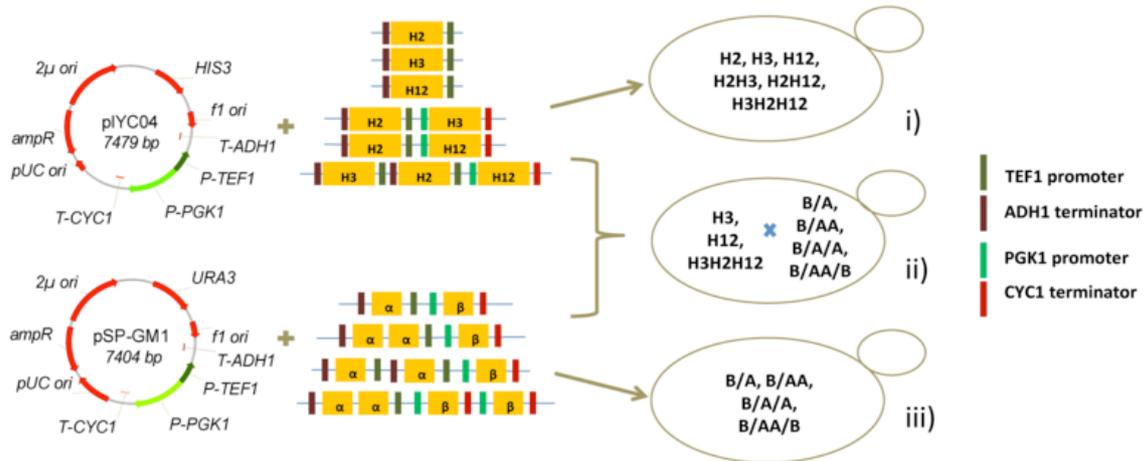
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523 Figure legend

524 Fig. 1. Engineering strategy for optimizing the production of human hemoglobin. (A) Strategy
525 overview: Yeast genes *HEM2*, *HEM3* and *HEM12* (highlighted in red) in heme biosynthesis pathway
526 were overexpressed for an improved level of heme in cell cytosol. Human α and β globins were
527 overproduced on plasmid in cytosol. Correct folding and assembling resulted in completed
528 hemoglobin, failure in assembling resulted in degradation. (B) Strain construction: CEN.PK 113-11C
529 as the expression host being transformed with i) heme overexpression plasmids: gene *HEM2*, *HEM3*
530 and *HEM12* were inserted into the expression cassette *TEF1-ADHI*, either individually or in different
531 combinations in the cassettes *TEF1-ADHI* and *PGK1-CYC1* on pIYC04. ii) globin overexpression
532 plasmids: *HBA*, *HBB*, and *HBAA* were inserted into pSP-GM1 in the cassettes of *TEF1-ADHI* and
533 *PGK1-CYC1* in different combinations. iii) heme and globin overexpression plasmids: The top three
534 best heme/coproporphyrin producing plasmids H3, H12 and H3H2H12 were transformed in different
535 combinations together with the globin overexpression plasmids B/A, B/AA, B/A/A and B/AA/B.
536 Hemoglobin structure was modified from (Lu et al., 2011). Heme biosynthesis pathway was modified
537 from (Hoffman et al., 2003)

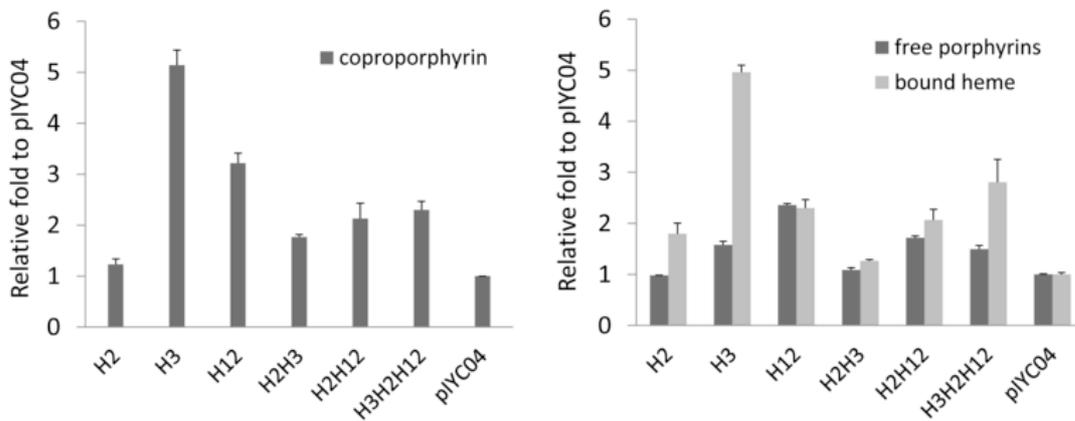


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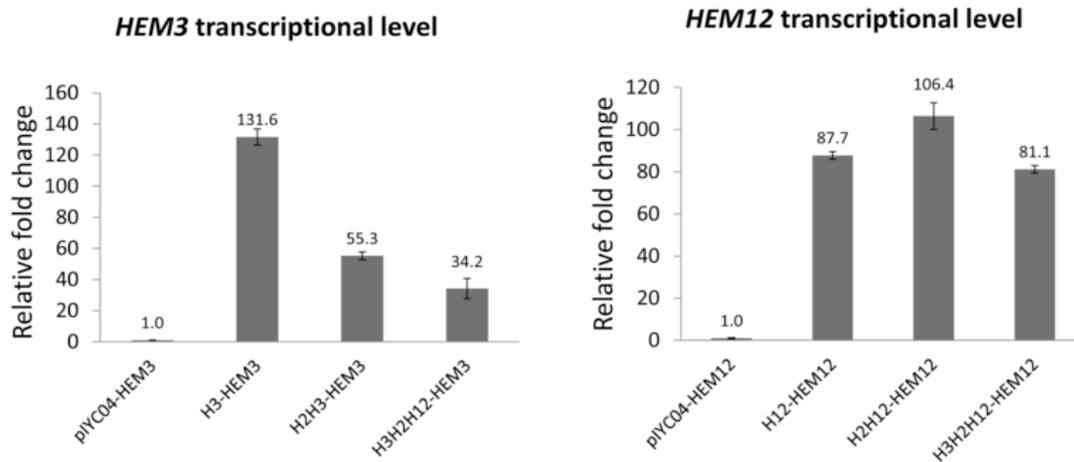
539

540 Fig. 2. Porphyrin/heme levels in heme over-expression strains. (A) Level of coproporphyrin. (B)
 541 Level of free porphyrins and bound heme. The relative fold change is calculated based on the
 542 fluorescence reads (excitation at $\lambda=400\text{nm}$ and emission at $\lambda=600\text{nm}$) of the sample strains against
 543 the control strain, pLYC04.



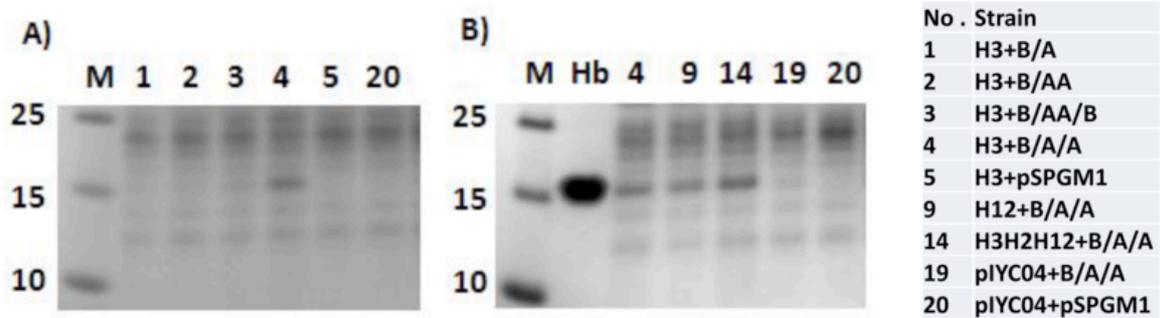
544

545 Fig. 3. Transcription level of (A) *HEM3* and (B) *HEM12* in the engineered strains transformed with
 546 Heme plasmids. In both cases, the relative fold change is calculated based on the transcription levels of
 547 the genes (relative to *ACT1*) in the sample strains against the control strain, pLYC04.



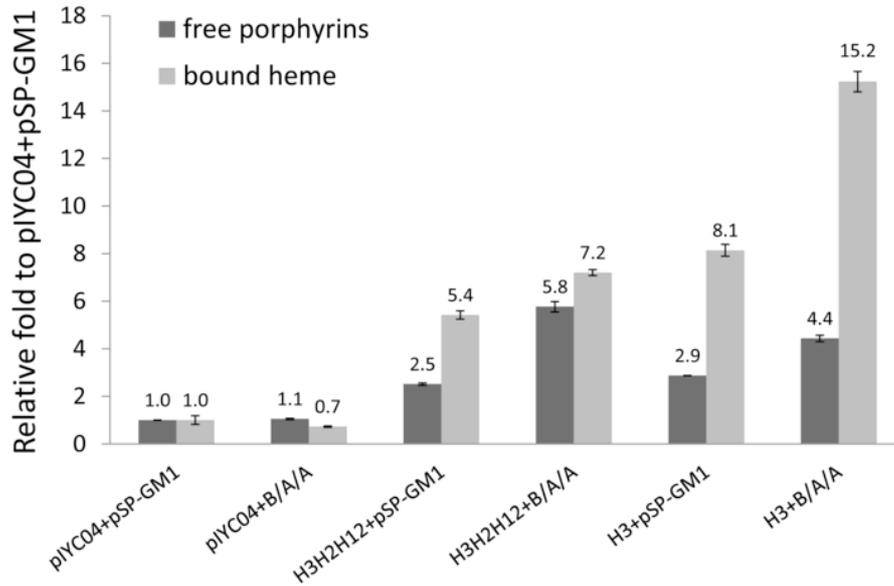
548

549 Fig. 4. SDS-PAGE analysis of the engineered strains with heme and globin co-overexpressed. (A) co-
 550 overexpression of H3 with the globin constructs. (B) co-expression of B/A/A with the heme constructs.
 551 M stands for the protein ladder, Hb stands for the standard hemoglobin (16 kDa) and the numbers
 552 indicate the strains listed in the table on the side. 50 μ g of total protein was loaded per lane.



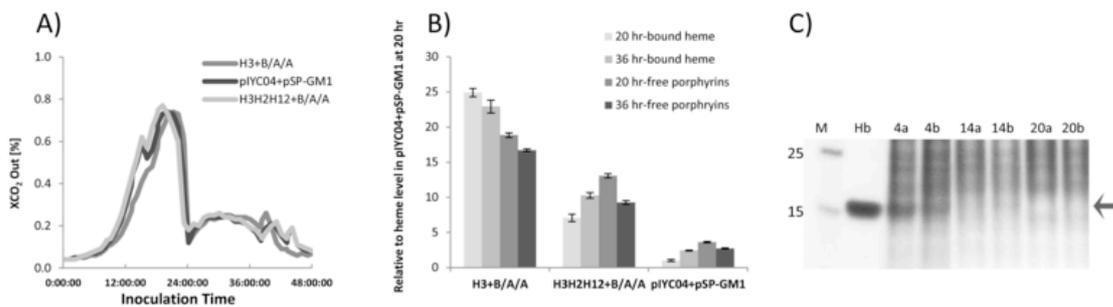
553

554 Fig. 5. Effects of B/A/A plasmid co-overexpression on heme/porphyrin level. The relative fold change
 555 is calculated based on the fluorescence reads (excitation at $\lambda= 400\text{nm}$ and emission at $\lambda= 600\text{nm}$) of
 556 the sample strains to that of the control strain, pIYC04.



557

558 Fig. 6. Heme and hemoglobin production during batch fermentations. (A) Offgas profile: showing that
 559 glucose phase finished at around 20 hrs and ethanol phase started at around 36 hrs. (B) Heme and
 560 porphyrin levels in strains after inoculation for 20 and 36hrs respectively. (C) SDS-PAGE analysis of
 561 the globin patterns produced at 20 and 36 hrs respectively. 4, 14, 20 represent strains H3+B/A/A,
 562 H3H2H12+B/A/A and pIYC04+pSP-GM1 respectively. a and b represent 20 and 36 hrs after
 563 inoculation. 25µg protein loaded.



564